- 1 Secondary organic aerosol reduced by mixture of atmospheric vapours 2 Gordon McFiggans<sup>1</sup>, Thomas F. Mentel<sup>2</sup>, Jürgen Wildt<sup>2,3</sup>, Iida Pullinen<sup>2,15</sup>, Sungah 3 Kang<sup>2</sup>, Einhard Kleist<sup>3</sup>, Sebastian Schmitt<sup>2,16</sup>, Monika Springer<sup>2</sup>, Ralf Tillmann<sup>2</sup>, 4 Cheng Wu<sup>2,17</sup>, Defeng Zhao<sup>5,2</sup>, Mattias Hallquist<sup>6</sup>, Cameron Faxon<sup>6</sup>, Michael Le 5 Breton<sup>1,6</sup>, Åsa M. Hallquist<sup>7</sup>, David Simpson<sup>8,12</sup>, Robert Bergström<sup>6,8,13</sup>, Michael E. Jenkin<sup>9</sup>, Mikael Ehn<sup>10</sup>, Joel A. Thornton<sup>11</sup>, M. Rami Alfarra<sup>1,14</sup>, Thomas J. Bannan<sup>1</sup>, 6 7 Carl J. Percival<sup>1,18</sup>, Michael Priestley<sup>1</sup>, David Topping<sup>1,14</sup>, Astrid Kiendler-Scharr<sup>2,4</sup> 8 9 10 1. University of Manchester, School of Earth and Environmental Sciences, Oxford Road, Manchester, M13 9PL, UK 11 12 2. Institut für Energie- und Klimaforschung, IEK-8, Forschungszentrum Jülich, 52425 13 Jülich, Germany 14 3. Institut for Bio- and Geosciences, IBG-2, Forschungszentrum Jülich, Jülich 52425, 15 Germany 16 4. I. Physikalisches Institut, Universität zu Köln, 50937 Köln, Germany 17 5. Department of Atmospheric and Oceanic Sciences & Institute of Atmospheric 18 Sciences, Fudan University, Shanghai, China 19 6. Atmospheric Science, Department of Chemistry and Molecular Biology, University 20 of Gothenburg, SE-41296 Gothenburg, Sweden 21 7. IVL Swedish Environmental Research Institute, PO Box 5302, SE-400 14 22 Gothenburg, Sweden 23 8. Department of Earth, Space and Environment, Chalmers University of 24 Technology, 41296 Gothenburg, Sweden 25 9. Atmospheric Chemistry Services, Okehampton, Devon, EX20 40B, UK 26 10. Institute for Atmospheric and Earth System Research / Physics, Faculty of 27 Science, University of Helsinki, P.O. Box 64, 00014, Helsinki, Finland 28 11. Department of Atmospheric Sciences, University of Washington, Seattle, 29 WA98195, USA 30 12. EMEP MSC-W, Norwegian Meteorological Institute, Oslo, Norway 31 13. Swedish Meteorological and Hydrological Institute, 60176 Norrköping, Sweden 32 14. National Centre for Atmospheric Science (NCAS), Oxford Road, Manchester, 33 M13 9PL, UK 34 15. Department of Applied Physics, University of Eastern Finland, 70211 Kuopio, 35 Finland 36 16. TSI GmbH, 52068 Aachen, Germany 37 17. Stockholm University, Department of Environmental Science & Analytic 38 Chemistry, SE-10691 Stockholm, Sweden 39 18. Jet Propulsion Laboratory, California Institute of Technology, Pasadena, CA 40 91109, USA
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42 Secondary organic aerosol contributes to the atmospheric particle burden with 43 implications for air quality and climate. Biogenic volatile organic compounds 44 emitted from plants are important secondary organic aerosol precursors with 45 isoprene emissions dominating globally. However, its yield of particle mass from oxidation is generally modest compared to that of other terpenoids. Here we show 46 47 that isoprene, carbon monoxide and methane can suppress the instantaneous mass 48 and the overall mass yield derived from monoterpenes in mixtures. We find that 49 isoprene scavenges hydroxyl radicals preventing reaction with monoterpenes and 50 the resulting isoprene peroxy radicals scavenge highly oxygenated monoterpene 51 products. These effects reduced the yield of low-volatility products that would 52 otherwise form secondary organic aerosol. Global model calculations indicate that 53 oxidant and product scavenging can operate effectively in the real atmosphere. 54 Highly reactive, modest aerosol yield compounds are not necessarily net producers 55 and their oxidation can suppress both particle number and mass.

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### 60 Introduction

The secondary organic fraction of fine aerosol is substantial<sup>1,2</sup> and contributes 61 significantly to the fine particulate matter (PM) burden<sup>3</sup> and aerosol impacts on 62 63 climate<sup>4</sup>. Conventionally, Secondary Organic Aerosol (SOA) particle mass is 64 considered to be formed independently from the condensable oxidation products of 65 each contributing volatile organic compound (VOC)<sup>5</sup>. The ambient atmosphere is a 66 complex mixture of biogenic and anthropogenic VOC, a limited number of which are normally considered to control the oxidant concentrations in air quality or climate 67 models<sup>4,5</sup>. Isoprene has been found to dominate plant VOC emissions globally<sup>6,7</sup>, 68 though it has been found only moderately effective at forming SOA particle mass<sup>8,9,10</sup>. 69 Nevertheless, isoprene oxidation tracers have been observed in particles in both 70 chamber experiments<sup>11,12</sup> and the atmosphere<sup>11,13,14,15</sup> showing that they condense from 71 72 the gas phase. Oxidation of the monoterpenes (MT), including  $\alpha$ -pinene, and sesquiterpenes is generally more efficient at producing SOA particle mass<sup>16,17,18</sup>. When 73 74 oxidation of a VOC contributing to SOA is explicitly considered in models, some 75 interaction between the oxidant field and the SOA formation process is implicit<sup>5</sup>, 76 though recently observed behaviour is yet to be described. Two such recent findings 77 have motivated the current work. First, it has been shown that C<sub>5</sub> isoprene molecules 78 suppress the nucleation of SOA particles in the oxidation of the C<sub>10</sub> MT in mixtures of plant emissions by successfully competing for the hydroxyl radical, OH<sup>19,20,21</sup>. Second. 79 80 recent direct observation of highly oxygenated organic molecules (HOM) formed from 81 MT oxidation<sup>22</sup>, and elucidation of the auto-oxidation mechanisms by which they are formed, have implicated them in the formation of new SOA particles. Our work moves 82 beyond the suppression of particle nucleation by isoprene using the new mechanistic 83 84 understanding to explain SOA mass and yield suppression in MT-containing mixtures. 85 These results highlight a need for more realistic consideration of SOA formation in the atmosphere analogous to the treatment of ozone formation, where interactions between 86 the mechanistic pathways involving peroxy radicals are recognised to be essential<sup>23</sup>. 87

#### 88 Use of SOA yields in mixtures

Ostensibly, the concept of a SOA yield is straightforward and unambiguous<sup>24-26</sup>. It has 89 90 been widely used to interpret the potential of precursor molecules to produce particulate 91 mass, most extensively from smog chamber studies and usually with the goal of 92 quantifying the formation of ambient atmospheric particles. Yield is normally defined 93 in terms of the particulate mass condensed for a given mass of gaseous parent VOC 94 consumed. The process of determining SOA yields presents substantial practical 95 challenges. Notwithstanding measurement uncertainties and artefacts (for example, 96 wall losses and those associated with the accurate determination of the mass of semi-97 volatile material<sup>27-31</sup>) there are numerous reasons why SOA yields may vary according 98 to the conditions under which they are measured. This paper does not aim to provide a 99 critical evaluation of the determination of SOA yields and their extrapolation to 100 atmospheric conditions and the reader is referred to a number of recent publications for a discussion of challenges and the state-of-the-science concerning the interpretation of 101 SOA formation from chamber experiments<sup>22,27,29-32</sup>. However, there are conceptual 102 103 aspects often implicit in the treatment of SOA formation either in chamber experiments, 104 real atmospheric mixtures, or models of the atmosphere that provide the context for the 105 current study.

106 First, the concept of yield frequently includes some assumption of equilibrium. An interpretation of particle mass in terms of the partitioning of components of known 107 108 volatility by absorptive partitioning invokes an equilibrium assumption. In reality, mass 109 takes a finite time to transfer between the continuous and dispersed phases<sup>33,34</sup>. Second, 110 a parent VOC will continue to react, as will its reaction products, provided they have 111 reaction partners. Under atmospheric, or simulated atmospheric, conditions the reaction 112 partners are normally oxidants, such as the hydroxyl radical OH (the main focus in this 113 paper). This means that the distribution of vapour phase components that is available 114 to transfer to the condensed phase by condensational growth or nucleation is 115 continuously evolving through photochemical reactions. Third, a yield integrates across 116 all oxidation products formed from the parent hydrocarbon, summing the fraction of 117 these products that will partition to the particle phase from whatever stage of oxidation 118 under the chosen reaction conditions. We further would like to note that the yields 119 themselves can be dependent on the oxidant concentration<sup>e.g.31,32</sup>.

120 This combination of characteristics raises first order challenges when considering SOA 121 formation in the real atmosphere which comprises a complex mixture of organic 122 vapours of widely varying volatilities, from numerous sources of anthropogenic and 123 biogenic origin. This paper is concerned with the challenge surrounding the 124 introduction of oxidants into the atmospheric mixture and the reactivity of the evolving components in the mixture – specifically, the yield of condensed organic particulate 125 126 material of any of the single component vapours in the mixture when it is consumed by 127 the oxidant. Any of the vapours may react with the available oxidant, so from the 128 perspective of any other vapour molecule, the oxidant has been "scavenged" and is 129 unavailable as a reaction partner. Our experimental systems illustrate the implications 130 on SOA formation of mixtures of precursors. We demonstrate how SOA yield in 131 mixtures is dependent on whether the reactivity of one of the SOA forming compounds 132 controls the oxidant and contrast conditions in the laboratory and the atmosphere. It is 133 not only the oxidants that can be removed from the system by components of a mixture. 134 The products from oxidation that can react to form the final condensable SOA 135 precursors may alternatively be scavenged by other reactive intermediates. This process 136 can form the basis for the reduction in yield of the individual components in a mixture, 137 as shown by our results below and detailed in the supplement sections.

### 138

## 139 Experiments to SOA formation in mixtures

140 In the Jülich Plant Atmosphere Chamber (JPAC; suppl. section 1) we find that the 141 presence of isoprene substantially suppresses the SOA mass formed from oxidation of 142  $\alpha$ -pinene, the most abundant MT in the atmosphere (Figure 1A). Furthermore, we show 143 that this reduction of SOA mass is not trivially due to the lower amount of MT 144 consumed in the presence of isoprene. Rather the presence of isoprene actually 145 suppresses the SOA mass yield from the amount of VOC consumed (Figure 1B). Isoprene thereby limits not only new particle formation<sup>19</sup> (hence exhibiting control over 146 147 particle number concentration) but also the growth of pre-existing particles and thus 148 their size. This has significant consequences for the abundance of PM mass formed in 149 the mixture and the number of particles that may grow to sizes where they can act as 150 cloud seeds. Our findings are surprising and unexpected in the context of existing 151 conceptions of SOA mass yields (suppl. section 2). As shown in Figure 1, the presence 152 of isoprene substantially suppresses the SOA mass formation from  $\alpha$ -pinene oxidation 153 by about 60% and the SOA yield by 40%. Figure S2 shows even greater suppression in 154 greater isoprene excess, with both mass and yield reduced in the presence of both 155 neutral and acidic seed. This contrasts sharply with current understanding, since isoprene oxidation should contribute substantially to SOA production when isoprene 156 157 concentrations are high.

158 Below we describe the two effects contributing to SOA suppression - oxidant 159 scavenging and product scavenging. This demonstrates the importance of accounting 160 for the reactivity of the parent VOC in atmospheric mixtures and hence their turnover 161 (suppl. section 2) as well as interactions between their reaction intermediates and 162 products. Whilst our experiments illustrate this requirement predominantly with 163 reference to the photochemical isoprene  $-\alpha$ -pinene system with OH as the major 164 oxidant, it should be noted that in all mixed systems investigated, OH (oxidant) 165 scavenging and product scavenging were found to reduce both the SOA particle mass and the SOA yield. Note that during daytime, both, ozonolysis and OH oxidation of  $\alpha$ -166 167 pinene, contribute to SOA, as in our experiments, however the contribution via OH reactions here was much greater than 90%. According to our mechanistic understanding 168 169 presented below, product scavenging will be similarly effective for OH and O<sub>3</sub> 170 oxidation.

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# 172 Oxidant and product scavenging

173 Oxidant scavenging is demonstrated by the decrease in SOA mass and yield of the 174 mixture with increasing isoprene fraction as well as by the decrease of the  $\alpha$ -pinene 175 yield itself (Figure 1B and suppl. section 3). The contribution of isoprene to SOA mass 176 in the presence of neutral ammonium sulfate aerosols is small and  $\alpha$ -pinene oxidation 177 products make up the overwhelming fraction of SOA in mixtures. Isoprene increasingly 178 efficiently competes with  $\alpha$ -pinene for the available OH as the reaction system is 179 stepped from high SOA yield pure  $\alpha$ -pinene to low SOA yield pure isoprene (Figure S2). With respect to  $\alpha$ -pinene, the isoprene "scavenges" the OH<sup>19</sup>, i.e. the steady state 180 181 OH concentration is lowered by the introduction of isoprene for a given OH source 182 strength, therefore less OH can react with  $\alpha$ -pinene, resulting in less SOA mass being formed. In addition, the SOA yield itself is dependent on  $[OH]^{31,32}$ . 183 184 By uniquely being able to control the OH at the same concentration with and without

185 isoprene addition by readjusting its source strength, we were able to reveal that the SOA

- mass (Figure 1A), and by implication the  $\alpha$ -pinene SOA yield (Figure 1B, 3<sup>rd</sup> bar), 186 187 decreased with increasing isoprene in the mixture (suppl. section 4). Strikingly, the  $\alpha$ -188 pinene SOA yield was reduced by 30% relative to the pure  $\alpha$ -pinene yield, even though 189 the OH scavenging effect has been removed ( $\Delta isoprene/\Delta \alpha$ -pinene $\approx 1\pm 0.2$  [ppb/ppb] = 190  $0.5\pm0.1$  [µg/µg]). Moreover, by re-adjusting [OH], we held the  $\alpha$ -pinene sub-system of the mixture at the same stage of oxidation as in the pure case. This results in the 191 192 condensing oxidation products having the same "chemical age" in both cases, thereby 193 avoiding comparison of chemical systems of different chemical evolution.
- 194 In Figure 2 we show the actual  $\alpha$ -pinene SOA yields (y<sub>act</sub>) in the mixture normalized to 195 the  $\alpha$ -pinene SOA yield  $v_{AP} = 17\%$  for pure  $\alpha$ -pinene in absence of isoprene. The  $v_{act}$ were calculated from the observed SOA mass and the actual consumption of  $\alpha$ -pinene. 196 197 Depending on the isoprene to  $\alpha$ -pinene ratio, SOA mass produced from the same 198 amount of consumed  $\alpha$ -pinene in the presence of isoprene can be reduced by more than 199 half compared to the amount formed when oxidised alone (Figure 2). Clearly, smaller 200 amounts of SOA forming products from α-pinene oxidation are formed in the presence 201 of isoprene – we denote this effect "product scavenging".
- The product scavenging effect (and the OH scavenging effect) on SOA formation is somewhat masked in the presence of the acidic seed aerosol with which isoprene has a significant yield<sup>12,35-37</sup> (suppl. section 4, Figure S3, Figure 1B, 6<sup>th</sup> bar). Replacing isoprene by CO shows, that the acidity of the seed particles did not affect the behaviour of  $\alpha$ -pinene (Figure S3), but indeed enhanced the isoprene contribution (Figure S4). This underlines the importance of liquid phase processes for isoprene, but also clearly shows that both scavenging effects are general phenomena in the gas phase.
- 209 SOA yield suppression also occurs when isoprene is mixed with  $\beta$ -pinene and when 210 CO or CH<sub>4</sub> were mixed with  $\alpha$ -pinene (suppl. section 5, Figures S5-S7, Figure 4). This 211 generality ensures that the influence of the relative reactivity of components in mixtures 212 on the SOA formation potential has much more profound implications than a simple 213 reduction in yield in each of the binary mixtures. Moreover, because of potential 214 interactions with additional SOA contributors, the yields in anything beyond the binary 215 mixtures cannot be simply added or in any way predicted without specific mechanistic 216 insight.
- The key to a mechanistic understanding of the product scavenging is the formation of HOM with the peculiarity that HOM peroxy radicals also dimerise in the gas phase<sup>38</sup> (suppl. section 6). It can be inferred from their structure and O/C ratios that HOM and even moreso their dimers, are low to extremely low volatility organic compounds<sup>22,39</sup> and will contribute substantially to SOA formation and initial growth<sup>22,39</sup>.
- 222 In Figure 3A we present direct observation of the product scavenging of  $\alpha$ -pinene HOM 223 by comparing mass spectra measured in OH reaction systems for  $\alpha$ -pinene-only and for 224 an  $\alpha$ -pinene/isoprene mixture. For  $\alpha$ -pinene-only we observed about equal signal 225 intensities in the ranges of  $\alpha$ -pinene HOM monomers with 10 C-atoms and of HOM 226 dimers with 17-20 C-atoms. In the presence of isoprene,  $\alpha$ -pinene dimers are 227 suppressed by a factor of about 3. Comparable dimer suppression by a factor of 2 is 228 observed for CO (Figure 4A). HOM dimers have been observed in the boreal ambient 229 atmosphere, lower during daytime than at night-time, but at lower fractions than in our  $\alpha$ -pinene-only experiments<sup>40,41</sup>. Since product scavenging will be occurring, 230 231 particularly during daytime, these observations are consistent with our findings.
- The strength of product scavenging is estimated by comparing two sets of experiments where the [OH] was tuned, either by varying the OH sink through adding different amounts of isoprene to the reaction system or by varying the OH production rate through modifying the photolysis rate  $J(O^{1}D)$  for O<sub>3</sub> (Figure 3B). With increasing

236 isoprene, the dimers are more strongly suppressed than with decreasing  $J(O^{1}D)$  as a 237 result of increased scavenging of a-pinene HOM peroxy radicals by isoprene related RO2 and HO2 radicals<sup>42</sup>. This leads to formation of less HOM, mainly by diminishing 238  $\alpha$ -pinene HOM self-dimerization. Suppression of the HOM dimers alone accounts for 239 27% reduction in HOM mass (Figure 3C) and explains most of the 35% SOA mass 240 reduction by the product scavenging effect shown in Figure 1, underlining the pivotal 241 role of HOM dimers in new particle and SOA formation<sup>22,39</sup>. The involvement of HOM 242 does not preclude the involvement of multigenerational oxidation as such (cf. suppl. 243 244 section 6). Indeed, the non-linear dependence of the total HOM on the turnover in 245 Figure 3B requires at least a second oxidation step and explains the dependence of the 246  $\alpha$ -pinene SOA yield on [OH], contributing to the OH scavenging effect.

247 The mechanism of product scavenging via dimer suppression by short chained peroxy 248 radicals or  $HO_2$  is general for peroxy radical chemistry and is not limited to the presence 249 of isoprene in the mixture. It is effective in mixtures of  $\alpha$ -pinene with CO via HO<sub>2</sub> 250 (Figure 4) and with CH<sub>4</sub> via CH<sub>3</sub>O<sub>2</sub> radicals (Figures S7). CO and CH<sub>4</sub> are extreme 251 cases, each with essentially no SOA yield. In both cases, the scavenging effects are 252 solely related to gas-phase chemistry and independent of aerosol composition: organic 253 or inorganic neutral or inorganic acidic particles. We therefore conclude that product 254 scavenging effect is a general effect in mixtures of VOC.

# 255

## 256 Atmospheric implications

257 Our new findings in JPAC would hold in atmospheric concentration regimes (suppl. 258 section 7). However, in the atmosphere, the OH concentration is not solely controlled 259 by the isoprene /  $\alpha$ -pinene ratio as in the JPAC chamber. Simulations using the EMEP MSC-W model<sup>43,44</sup> (suppl. section 8) show that the scavenging effects by isoprene 260 261 under realistic atmospheric conditions lowers the OH concentration compared to the 262 hypothetical "no isoprene" case and affects the SOA formation. However, even at small 263 isoprene SOA yields, the gains of isoprene SOA and MT-O<sub>3</sub>-SOA offset the reduction 264 from OH scavenging (Figure 5, noIso, OHS). When a parameterisation of the product 265 scavenging constrained to our measurements (Figure 2) is included in the global model simulations, we find that photochemically generated MT-OH-SOA is strongly 266 267 suppressed, in areas with sufficiently high MT and isoprene emissions (Figure 5, PS). 268 The dramatic effects on MT-OH-SOA show the potential for product scavenging to 269 reduce aerosol loadings substantially in many regions of the world, even more so if one 270 considers that product scavenging similarly could also affect e.g. the MT-O3-SOA 271 (Figure 5, PSox). It is not possible to be so sure about the magnitude of OH scavenging 272 from all potential reactants, since more measurement constraint is needed to include 273 mechanistic descriptions in such systems.

274 Extending our results from mixtures of isoprene, CH<sub>4</sub>, and CO with  $\alpha$ -pinene or  $\beta$ -275 pinene to the reactive atmospheric mixture of vapours, any of the reaction products 276 from any of the components in the mixture may react together, such that from the 277 perspective of any of the others, they have been "scavenged" from the mixture. 278 Similarly, from the perspective of the formation of organic particulate material, some 279 of the condensable oxidation products that are direct precursors may be "scavenged", 280 in all cases reducing the ambient yield. Spatial distribution of short chain organic 281 compounds and specific composition of the reaction mixture will determine the strength of the OH and the product scavenging effects. Whilst long lived compounds, like CH4, 282 283 may act ubiquitously in cleaner regions of the earth, compounds with strong 284 anthropogenic sources, like CO, may not exert their full scavenging potential because, 285 when high in concentration, they are always accompanied by high concentrations of 286 other pollutants, like NOx. While oxidant scavenging will take place under nearly all 287 conditions, product scavenging across SOA precursors is a complex function RO2terminating agents, such as peroxy radicals of VOC with moderate or no SOA yield, 288 289 HO<sub>2</sub>, and NO<sub>X</sub>. Product scavenging and "non-additivity" of SOA yields will thus vary 290 from region to region, accordingly. Without further experimentally constrained parameterisation of the interactions between all relevant components in realistic 291 292 atmosphere, it is not possible to predict the magnitude and geographical distribution of 293 suppression of SOA formation. Inclusion of explicit interactions of such complexity in 294 global simulations is practically impossible. It is only possible to say for the considered 295 systems that the SOA yields and net SOA mass must be reduced compared to linear 296 addition of yields, even if the control of oxidant were realistically included.

297

# 298 Outlook and recommendations

299 Our findings demonstrate that SOA precursors with modest yields suppress SOA 300 forming products of higher SOA yield precursors substantially. Our work directly challenges two widespread treatments of SOA formation and suggests an alternative 301 302 mechanistically-based solution. A first obvious recommendation following this work is 303 that the decoupling of the modulation of oxidant fields from SOA precursor turnover is 304 clearly discouraged. We have further demonstrated that simple linear addition of SOA 305 mass from the individual yields of components in a VOC mixture will likely lead to a 306 substantial overestimation of SOA production. Measuring SOA yields with individual 307 compounds leads to insight into the mechanisms of SOA production but the results do not reflect the conditions of the real environment. Such data should therefore be used 308 309 with caution when modelling aerosol formation. In the general case, the abundance of 310 HOM, HOM-RO2 and RO2 products from potential SOA precursors as well as from 311 volatile compounds not producing SOA mass should be considered when predicting the 312 mixture's yield. Our results highlight a need for more realistic consideration of SOA 313 formation in the atmosphere analogous to the treatment of ozone formation, where interactions between the mechanistic pathways involving peroxy radicals are 314 recognised to be essential<sup>23</sup>. It may be possible to produce lumped classes of precursors 315 according to their likelihood of increasing or decreasing a mixture's yield and this could 316 317 be a focus of further investigation.

It is likely that both background oxidant concentrations and VOC emissions (and henceOH reactivity) will change in the future. Without a reasonable representation of SOA

320 yields in different atmospheric VOC mixtures it will not be possible to achieve

- 321 predictive capability for the SOA contribution to particulate matter.
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# 474 **Author contributions:**

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- 482 All co-authors discussed the results and commented the manuscript and the supplement.
- 483

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# 503 Data availability statements

All data used are shown as Figures or Tables in the manuscript or in the supplemental information. Raw data are available from the corresponding author on reasonable request.

# 508 Figure Captions

509

510 Figure 1: Reduced SOA mass and yield of  $\alpha$ -pinene by product scavenging and OH scavenging by isoprene.

512 The top panel depicts symbolically the transition of the reaction system. a: Neutral seed 513 particles: isoprene (red triangles) lowered [OH] (black diamonds) and the 514 corresponding consumption of  $\alpha$ -pinene (blue squares), reducing the organic mass 515 dramatically. The organic mass was normalized to sulfate mass (organics/SO<sub>4</sub><sup>2-</sup>, green 516 circles). The newly discovered product scavenging (red) in the presence of isoprene is 517 separated from OH scavenging (orange) by re-adjustment of [OH]. Because of product 518 scavenging only 60% of the organic mass is formed despite the same  $\alpha$ -pinene 519 consumption. (The acidic case is depicted in Figure S3.) Vertical error bars for  $\Delta \alpha$ -520 pinene and  $\Delta$  isoprene are s.d. for averaging 14-15 samples, horizontal bars show the 521 averaging intervals. For OH we estimate an overall error of  $\pm 33\%$ .

522 b: The SOA yields in presence of neutral ammonium sulfate (blue) and acidic 523 ammonium bisulfate (red) seed particles were calculated at times B, C, and, D as 524 organic mass/ $\alpha$ -pinene consumption (acidic seed particles, see suppl. section 3). Not 525 only the SOA mass (indicated by the green spheres in the middle) but also its yield 526 decreased strongly (bar plots). B shows the SOA yield for a-pinene alone, while C 527 shows the summed effect of the new product scavenging and OH scavenging in the α-528 pinene & isoprene reaction system. For the neutral seeds D demonstrates the magnitude 529 of the product scavenging effect on the SOA yield, as [OH] and α-pinene consumption 530 were re-adjusted to the same levels as before isoprene addition. On acidic seed aerosol 531 (red) isoprene makes a substantial contribution to SOA, which compensates for some 532 of the OH scavenging effect and most of the product scavenging effect. The errors 533 reflect the estimated overall 15% uncertainty for an individual experiment.

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536 **Figure 2:** The reduction of the SOA yield of  $\alpha$ -pinene by isoprene as a function of the 537 isoprene/ $\alpha$ -pinene consumption ( $\Delta$ isoprene/ $\Delta\alpha$ -pinene).

538 The actual SOA yield of  $\alpha$ -pinene (y<sub>act</sub> =  $\Delta$ organic mass /  $\Delta \alpha$ -pinene) in  $\alpha$ -pinene & 539 isoprene mixtures was normalized to the average SOA yield obtained with a-pinene-540 only (y<sub>AP</sub>) at same conditions for neutral (blue) and acidic seeds (red). The grey area 541 indicates the  $\pm 20\%$  band for the scattering of the  $\alpha$ -pinene-only yields around y<sub>AP</sub> = 542 0.17 which includes the 15% error in the individual SOA mass yields (vertical bars) 543 and the variability of the experimental conditions for the reaction system with a-pinene-544 only. Horizontal error bars show the uncertainties of the isoprene/ $\alpha$ -pinene ratio (±10%) 545 derived from the measurement errors of the compounds.

546 The dashed line is the fit to the results for the neutral seeds that was implemented in the 547 global model calculations to parametrize product scavenging:

- 548  $y_{act} = y_{AP} \cdot (0.48 + 0.52 \cdot exp[-1.53 \cdot (\Delta isoprene / \Delta \alpha pinene)])$
- 549
- 550

551

552 **Figure 3:** HOM monomer/dimer distribution in the presence and absence of isoprene 553 illustrating the product scavenging effect.

554 a: comparison of two mass spectra taken in experiments with (orange) and without 555 isoprene (blue). In the presence of isoprene the dimer/monomer drops to about 1/3, indicating that the formation of these extremely low vapour pressure compounds is 556 557 efficiently suppressed in the presence of isoprene. b: Both the total HOM 558 (monomers+dimers, circles) and HOM dimers (squares, molecular mass > 370 Da) decrease with decreasing a-pinene turnover. Here [OH] was varied in two different 559 560 ways: i) by decreasing the OH production rate, i.e. by decreasing the photolysis of 561 ozone (J(O<sup>1</sup>D), blue) and ii) by adding increasing amounts of isoprene (red). In the presence of isoprene HOM decrease more strongly, mainly because the product 562 563 scavenging is suppressing the  $\alpha$ -pinene HOM dimers. The total HOM from the two different experiments were normalized to 1 for better comparison. c: Estimate of the 564 565 product scavenging effect on  $\alpha$ -pinene HOM dimers by isoprene at turnover 5.0x10<sup>7</sup> 566 cm<sup>-3</sup> s<sup>-1</sup> based on molecular mass weighted signals in the mass spectra (details in Figure S8). Data for  $\alpha$ -pinene-only were interpolated from the nearest J(O<sup>1</sup>D) data (arrows in 567 568 **b**). The reduction in total HOM mass is 33%, to which dimers (dark green) contribute 569 26% and monomers 7% (light green). Error bars show the s.d. of the averages over 31 570 data points. The suppression of  $\alpha$ -pinene HOM dimers of 26% explains most of the 571 35% product scavenging derived from reduced SOA formation in Figure 1. The balance 572 is a result of the reduced yield of HOM monomers and/or shifts in their volatility 573 spectrum.

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576 Figure 4: Suppression of  $\alpha$ -pinene SOA in presence of CO illustrating the generality 577 of the product scavenging effect.

a: comparison of three mass spectra taken in experiments with (orange [CO]=10 ppm, 578 579 red [CO]=57 ppm) and without CO (blue). In the presence of [CO] > 10 ppm the 580 dimer/monomer drops by more than 1/2, indicating that the formation of the dimers is 581 efficiently suppressed in the presence of CO. Because of the high [CO] overall HOM 582 are suppressed by factor of 4 and 5 respectively. b: The product scavenging effect 583 reduces the  $\alpha$ -pinene yield in the reaction system  $\alpha$ -pinene & CO & OH in the presence 584 of ammonium sulfate seeds. The actual SOA yield, calculated as actual organic 585 mass/actual  $\alpha$ -pinene consumption, decreases by more than 50%, when 40 ppm CO was 586 added to the reaction system. CO concentrations were calculated from known inlet 587 concentration, the flow rate through the RC and the reaction rate of CO with OH. Light 588 colored data points show steady state averages, whereby horizontal error bars show the 589 averaging interval; s.d. of the averages are of the same size or smaller than the symbols. 590 Note, panels **a** and **b** were not taken from the same experiment: experiments to show 591 HOM in the gas-phase and to show SOA suppression cannot be performed in optimal 592 fashion under the same conditions. To measure the unperturbed HOM-MS, particle 593 formation must be avoided. In contrast, mass formation and its suppression must be 594 determined in presence of seed surface as HOM losses at the walls of the chamber have 595 to be minimized. Therefore, the experiment to measure the HOM-MS was performed 596 without seed aerosol whereas ammonium sulfate particles were added to measure the 597 suppression of mass formation by CO. Otherwise the conditions of the experiments 598 were similar.

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- 600

601 **Figure 5**: Atmospheric implications of product scavenging and OH scavenging.

602 Global model calculations showing that OH scavenging (OHS) and product scavenging

603 (PS) in presence of isoprene reduce the photochemically derived MT-OH-SOA mass

604 (red) significantly compared to the reference cases NoIso. For the calculation a 4% 605 iSOA yield for acidic aerosols was applied (sum of the brownish bars). OHS is

606 inherently considered in models as long as biogenic SOA (BSOA) formation is directly

607 linked to the oxidant fields, but the new PS effect reduces the MT-OH-SOA even

608 further. To illustrate the maximum potential PS effect it was also applied to ozone

derived MT-O<sub>3</sub>-SOA (orange, PSOx). In this case the iSOA gain for 1% iSOA yield on

610 neutral aerosols (dark brown) would not be able to compensate for the loss of MT-SOA.

611 We show the global average and results for regions with high and low isoprene

emissions and high and low population density. The map shows isoprene emissions,

613 green shaded in  $[mg m^{-2}]$  and the areas of the selected regions. All contributions are 614 normalised to MT-OH-SOA of the respective NoIso case, when biogenic isoprene

615 emissions were omitted in the model (suppl. section 8).



Normalized actual  $\alpha$ -pinene yield in the mixture











#### Supplement to

### Secondary organic aerosol reduced by mixtures of atmospheric vapours

### 1. Jülich Plant Atmosphere Chamber (JPAC)

The experiments were performed in a continuously stirred flow reactor with a volume of 1450 L, which is part of the Jülich Plant Atmosphere Chamber (JPAC). The reaction chamber (RC) is located in a thermally stabilised housing and was used in the latest extension stage as described previously<sup>22,45,46</sup> and sketched in Figure S1. In short: supply air was pumped through the RC at a total flow of 30-35 L min<sup>-1</sup> resulting in a residence time of 40-50 min. The supply flow was split into half onto two separate lines for the reactants in order to prevent reactions in the supply lines. Ozone and water vapour were added to one of the air streams entering the RC, while the other inlet stream contained the VOC. Here we studied  $\alpha$ -pinene (Aldrich, purity > 99%) and isoprene (Aldrich, purity > 99%) and mixtures of both. VOC,  $\alpha$ -pinene and isoprene, were introduced into the RC by flowing clean nitrogen over diffusion sources<sup>47</sup>. Since we prepare the clean air by purifying outside air including catalytic combustion, there is always a residual NO<sub>X</sub> concentration of about 300 ppt in the RC. Here, all experiments were performed under low NO (NO < 30ppt) and low NO<sub>2</sub> (NO<sub>2</sub> < 300ppt) conditions. Steady state concentrations of the VOC during the experiments are given in Table S1. In few accompanying experiments we used  $\beta$ -pinene (Aldrich, purity > 99%), CO (Prüfgas, 4000 ppm in  $N_2$ , Linde AG) and CH<sub>4</sub> (purity, 99.9995 %, Linde AG).

OH radicals were produced by  $O_3$  photolysis at 254 nm in the presence of water vapour. The forming excited  $O^1D$  atoms react with water vapour in the chamber and generate OH radicals in a concentration range of  $1-10 \cdot 10^7$  cm<sup>-3</sup>. The OH concentration [OH] is regulated by the source strength i.e. by shielding the UV light shining into the chamber by two movable glass shields which are opaque to light at 254 nm allowing for different length of the open gap of the UV. The actual OH steady state concentration [OH]<sub>ss</sub> depended also on the VOC source strength, i.e. even if  $O_3$  flow into the chamber and TUV gap were held constant,  $O_3$  steady state concentration and OH concentration varied depending on the reactivity provided by  $\alpha$ -pinene, isoprene, and their mixtures. The [OH]<sub>ss</sub> are listed in Table S1.

Several instruments were used to measure the chamber experiment conditions. Ozone was measured by two UV photometric devices: Thermo Environment 49 or Ansyco, O3 42M ozone analyser. To monitor humidity dew point mirrors were used at both inlet and outlet flows. All instruments could be switched from outlet to inlet to follow the differences caused by reactions in the chamber.



Figure S1: Schematic of the JPAC Reaction Chamber (RC).

 $\alpha$ -pinene and isoprene were introduced to the RC by flowing clean nitrogen over diffusion sources. Ozone and water, in separate flows, provided O<sub>3</sub> concentrations around 60 ppb and relative humidity of about 60% at 15°C. The total flow amounted to 30 L/min, resulting in a residence time of about 50 min. in the RC of 1450L volume. Concentrations of  $\alpha$ -pinene and isoprene, as well as oxidations products, were measured at inlet and outlet of the RC by GC-MS and PTR-MS. By switching on the UV lamp, O<sub>3</sub> was photolysed and O<sup>1</sup>D atoms reacted with water vapour to give OH at concentrations in a range of 1-10·10<sup>7</sup> cm<sup>-3</sup>. The OH source strength was regulated by the two movable glass shields allowing for different length of the gap for the UV. HOM were detected by a NO<sub>3</sub><sup>-</sup>-TOF-CIMS directly under the RC. Particle number concentration and number size distribution were determined by a Condensation Particle Counter (CPC) and by a Scanning Mobility Particle Sizer (SMPS). The particle composition was measured by an aerosol mass spectrometer (HR-TOF-AMS).

The number concentration of particles and their number size distribution were measured at the outlet of the RC by a CPC (TSI 3783) and by an SMPS (TSI 3081 electrostatic classifier combined with TSI 3025 CPC). Particle composition was measured using a high-resolution time of flight aerosol mass spectrometer (HR-ToF-AMS). A modified version of the HR-ToF-AMS (Aerodyne Inc., hereafter referred to as AMS) was used<sup>48</sup>. Briefly an AMS allows the mass spectrometric online investigation of aerosol particle composition after substantial reduction of the gas phase. The AMS was calibrated for ionization efficiency with NH<sub>4</sub>NO<sub>3</sub> and (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> aerosol and particle size calibrated using polystyrene latex standards (PSL, Duke Scientific Corporation, Palo Alto CA) of different sizes between 81 nm and 596 nm. Compound specific relative ionization efficiencies (RIE; ionization efficiency relative to NO<sub>3</sub><sup>-</sup>) were used. For NH<sub>4</sub><sup>+</sup> and SO<sub>4</sub><sup>2-</sup>, RIE was determined from the respective calibration close to each experiment and was

found to be in the range of 3.75 - 4.2 and 0.83 - 1.03, respectively. RIE for particulate water was set to  $2.0^{49}$ . The RIE for organics was kept at the standard value of  $1.4^{50}$ . For the determination of the collection efficiency (CE) the volume concentration was calculated from SMPS measurements and multiplied by a density to yield the mass concentration. The density was calculated from the relative ratios of ammonium sulfate (density= $1.77g \text{ cm}^{-3}$ ), particulate water (density=1 g cm<sup>-3</sup>) and organics (density= $1.4 \text{ g cm}^{-3}$ ). The ratio of total measured mass from AMS (sum of organics, sulfate, ammonium and particulate water) to mass derived from SMPS gave then the respective CE. The CE was between 0.2 and 0.3 since the ammonium sulfate mass fraction of the aerosol phase was typically > 60%. An average CE was determined and applied for each experiment. The data analysis focused on the mass concentration of the organic fraction and the organic/SO<sub>4</sub> ratio.

Highly oxygenated multifunctional molecules (HOM) are formed in the gas-phase in the RC by OH reaction and ozonolysis of  $\alpha$ -pinene. HOM were measured by an Atmospheric Pressure interface High Resolution Time of Flight Mass Spectrometer (APi-TOF-MS, Aerodyne Research Inc. & Tofwerk AG)<sup>51</sup>. The anion NO<sub>3</sub><sup>-</sup> is able to form a cluster with the expected HOM.<sup>52</sup> Therefore the APi-TOF-MS was equipped with a NO<sub>3</sub><sup>-</sup>-Chemical Ionization (CI) source<sup>53,54</sup> (A70 CI-inlet, Airmodus Ltd). The NO<sub>3</sub><sup>-</sup>-TOF-CIMS was directly placed under the RC within the thermo-stabilised housing of the chamber, i.e., it was operated at stable temperature conditions. Reagent ions <sup>14</sup>NO<sub>3</sub><sup>-</sup> were formed from HNO<sub>3</sub> (Merck) ionized by an in-line <sup>241</sup>Am foil. The vial with the nitric acid and all lines were also placed within the thermo-stabilised housing.

The length of sampling line (ID 8 mm) was about 30 cm and the sample flow from the RC into the CI source was 10 L/min. The flow into the NO<sub>3</sub><sup>-</sup> TOF-CIMS was thereafter reduced to 0.8 L/min by passing a critical orifice. Differential pumping by a scroll pump and a three-stage turbo pump decreased sequentially the pressure from 1015 mbar in the CI region to  $10^{-6}$  mbar in the Time of Flight region. After passing the critical orifice the ions are guided by segmented quadrupole mass filters and electrical lenses in the TOF extraction region. Collisions between ions and gas molecules will take place, but the energies are tuned low enough that only weakly bound clusters (e.g. water clusters) will fragment. After extraction into the TOF region the ions are separated by their different flight times depending on their mass-to-charge (*m/z*) ratio.

There is strong indication that the sensitivity of the  $NO_3$ -TOF-CIMS is fairly similar for all HOM species once a certain degree of functionalization is achieved (two –OH or –OOH groups in addition to two carbonyl groups)<sup>22,55</sup>

Studies with cyclopentane showed that HOM with 5 C atoms and 6 O atoms or more can be detected. However, we are able to detect HOM with less than 6 O-atoms in molecules with 7 or more C-atoms<sup>45</sup>. Thus, the polarisability of a molecule may play a role in addition to directional interactions of functional groups with the  $NO_3^-$  ion.

∆lsoprene [µg] ∆α-Pinene [µg]	[OH] [cm <sup>-3</sup> ]	Mixing ratio α-pinene in RC [ppb]	α-pinene consumption [µg m <sup>-3</sup> ]	Isoprene consumption [µg m <sup>-3</sup> ]	Organic mass [µg m <sup>-3</sup> ]	Particle Surface S <sub>tot</sub> [m <sup>2</sup> m <sup>-3</sup> ]	Wall loss corr. factor 1/F <sub>pHOM</sub>	Corr. organic mass [µg m³]	Yield iso.+α-pin.	Yield α-pin
α-pinene only										
neutral seeds										
-	$7.1 \cdot 10^7 \pm 6.9 \cdot 10^6$	1.2	68 ± 0.7	0	5.8	2.660·10 <sup>-4</sup>	1.768	10.3	-	0.152
-	$3.2 \cdot 10^7 \pm 1.6 \cdot 10^6$	2.1	56 ± 1.2	0	6.3	4.157·10 <sup>-4</sup>	1.529	9.6	-	0.172
-	$3.6 \cdot 10^7 \pm 2.3 \cdot 10^6$	1.9	55 ± 1.9	0	6.6	3.166·10 <sup>-4</sup>	1.646	10.9	-	0.197
-	$7.1 \cdot 10^7 \pm 7.8 \cdot 10^6$	1.1	64 ± 2.3	0	8.3	8.472·10 <sup>-4</sup>	1.241	10.3	-	0.162
-	$4.9 \cdot 10^7 \pm 5.1 \cdot 10^6$	1.5	65 ± 2.0	0	7.2	8.451·10 <sup>-4</sup>	1.251	9.0	-	0.138
-	$4.8 \cdot 10^7 \pm 4.6 \cdot 10^6$	1.5	61 ± 3.0	0	6.5	8.451·10 <sup>-4</sup>	1.241	8.1	-	0.133
-	$4.0 \cdot 10^7 \pm 3.0 \cdot 10^6$	1.8	60 ± 2.7	0	13.3	1.878·10 <sup>-3</sup>	1.113	14.8	-	0.246
-	$2.4 \cdot 10^7 \pm 3.5 \cdot 10^6$	2.8	53 ± 3.1	0	8.8	1.340·10 <sup>-3</sup>	1.152	10.1	-	0.190
-	$2.7 \cdot 10^7 \pm 5.4 \cdot 10^6$	2.5	55 ± 2.3	0	9.6	1.482·10 <sup>-3</sup>	1.138	10.9	-	0.197
acidic seeds										
-	$1.0 \cdot 10^8 \pm 1.9 \cdot 10^7$	0.8	68 ± 2.5	0	8.1	1.102·10 <sup>-3</sup>	1.186	9.7	-	0.142
-	$4.4 \cdot 10^7 \pm 6.3 \cdot 10^6$	1.7	61 ± 1.0	0	10.7	1.344·10 <sup>-3</sup>	1.152	12.3	-	0.201
a-pinene & isoprene	-									
neutral seeds										
0.35	2.8·10 <sup>7</sup> ± 2.0·10 <sup>6</sup>	2.4	55 ± 2.7	19 ± 0.2	3.7	6.399·10 <sup>-4</sup>	1.318	4.9	0.066	0.090
0.61	7.9·10 <sup>6</sup> ± 6.1·10 <sup>5</sup>	5.7	37 ± 1.3	23 ± 0.8	3.6	1.287·10 <sup>-3</sup>	1.158	4.2	0.070	0.113
0.47	$2.3 \cdot 10^7 \pm 4.3 \cdot 10^6$	3.0	57 ± 2.0	27 ± 3.3	2.8	1.431·10 <sup>-4</sup>	2.404	6.6	0.079	0.116
0.51	2.3·10 <sup>7</sup> ± 1.9·10 <sup>6</sup>	2.8	53 ± 0.9	27 ± 0.4	6.4	1.406·10 <sup>-3</sup>	1.144	7.3	0.090	0.136
0.53	$3.4 \cdot 10^7 \pm 1.7 \cdot 10^6$	2.2	62 ± 0.5	33 ± 0.3	3.3	1.810·10 <sup>-4</sup>	2.131	7.1	0.075	0.115
1.36	$1.1 \cdot 10^7 \pm 7.4 \cdot 10^5$	4.8	41 ± 2.3	56 ± 0.5	5.1	1.390·10 <sup>-3</sup>	1.147	5.9	0.061	0.143
1.39	$1.3 \cdot 10^7 \pm 8.7 \cdot 10^5$	4.2	43 ± 1.9	60 ± 0.7	4.4	3.802·10 <sup>-4</sup>	1.550	6.9	0.067	0.160
1.83	9.0·10 <sup>6</sup> ± 7.1·10 <sup>5</sup>	5.3	38 ± 3.0	70 ± 1.5	1.7	6.575·10 <sup>-4</sup>	1.311	2.2	0.021	0.058
2.64	1.1·10 <sup>7</sup> ± 1.1·10 <sup>6</sup>	4.8	40 ± 3.0	105 ± 0.6	1.9	7.496·10 <sup>-4</sup>	1.271	2.5	0.017	0.062
3.70	$7.0 \cdot 10^6 \pm 4.3 \cdot 10^5$	6.0	30 ± 1.7	110 ± 1.4	1.8	3.114·10 <sup>-4</sup>	1.680	3.0	0.022	0.102
6.68	$2.7 \cdot 10^6 \pm 3.2 \cdot 10^5$	8.8	20 ± 3.3	137 ± 13.3	0.8	6.413·10 <sup>-4</sup>	1.318	1.0	0.007	0.050
acidic seeds	•									
0.48	$4.3 \cdot 10^7 \pm 4.0 \cdot 10^6$	1.7	61 ± 1.1	29 ± 0.2	15.2	1.489·10 <sup>-3</sup>	1.137	17.2	0.191	0.282
0.50	1.3·10 <sup>7</sup> ± 1.2·10 <sup>6</sup>	4.4	46 ± 2.9	23 ± 0.4	7.3	1.315·10 <sup>-3</sup>	1.155	8.4	0.122	0.183
0.85	n.a.	4.7	46 ± 1.0	39 ± 0.4	4.5	1.034·10 <sup>-3</sup>	1.205	5.5	0.065	0.120
2.74	$3.6 \cdot 10^7 \pm 2.3 \cdot 10^6$	11.3	57 ± 3.2	155 ± 2.2	5.9	6.915·10 <sup>-4</sup>	1.369	8.1	0.038	0.143
6.77	$7.1 \cdot 10^7 \pm 7.8 \cdot 10^6$	14.2	40 ± 2.7	272 ± 8.4	4.7	6.600·10 <sup>-4</sup>	1.386	6.5	0.021	0.161

### Table S1: Overview of a-pinene and a-pinene + isoprene experiments

To control whether or not peaks in the NO<sub>3</sub><sup>-</sup>TOF-CIMS mass spectra originated from oxidation of the added VOC, blank experiments without VOC addition were performed. Ozone was left in the chamber in case of peaks originating from ozonolysis of impurities. Some of the peaks in the mass spectra were abundant also in absence of VOC and likely arise from fluorinated contaminants. All peaks observable without VOC addition were excluded from interpretation.

VOC and their oxidation products were measured by a high sensitivity Proton-Transfer-Reaction Mass-Spectrometer (PTR-MS, IONICON). The technique is described in the literature<sup>56</sup>. Calibrations for  $\alpha$ -pinene and isoprene were performed by using diffusion sources<sup>57</sup>. The PTR-MS was operated at 2 min time resolution and switched every 25 min between the inlet and the outlet of JPAC. The sampling lines consisted of ~10 m long PFA tubing of 4 mm inner diameter and were heated to 60°C. The sampling flow rate was 500 mL/min. The difference between inlet and outlet signal for  $\alpha$ -pinene at *m/z* 137 was used to determine the OH concentration.

Most of the experiments were performed in the presence of seed particles to provide surfaces for condensing the oxidation products of  $\alpha$ -pinene and isoprene in order to overcome the nucleation

barrier for secondary organic aerosol formation. The seed aerosols were generated by a TSI 3076 constant output aerosol generator with subsequent drying to RH<30% by diffusion dryers filled with silica gel. As neutral seeds we used ammonium sulfate particles, which were generated by spraying an aqueous ammonium sulfate solution. Acidic seeds were generated by spraying ammonium bisulfate solutions which were doped with some  $H_2SO_4$  to guaranty acidity. The latter was assured by monitoring the molar  $NH_4/SO_4$  ratio being <1 by AMS. In the evaluation of the seeded experiments the organic fraction of the aerosols observed by AMS was normalized to sulfate in order to correct for fluctuations of the particle concentration thus the condensation sink in the RC. Fluctuations arose from the long term instabilities in the particle generation process. Experiments for studies of the gas-phase composition were performed in absence of seed aerosols.

Because of the vigorous ongoing debate in the literature about the yield of isoprene and its role for SOA formation (e.g.<sup>58</sup> and references therein), we performed also experiments with isoprene only. An overview of the experiments with neutral and acidic seeds is given in Table S2. We refer to isoprene yields determined in our setup in the following discussions.

Experiment Qualifier	[OH] [cm <sup>-3</sup> ]	Mixing ratio isoprene in RC [ppb]	lsoprene consumption [µg m <sup>-3</sup> ]	Organic mass [µg m <sup>-3</sup> ]	Particle Surface S <sub>tot</sub> [m <sup>2</sup> m <sup>-3</sup> ]	Wall loss corr. factor 1/F <sub>pHOM</sub>	Background offset [µg m <sup>-3</sup> ]	Corr. organic mass [µg m <sup>-3</sup> ]	Yield corrected
isoprene neutral seeds									
1	$2.4 \cdot 10^7 \pm 6.7 \cdot 10^5$	10.3 ± 0.2	139.0 ± 0.7	2.48 ± 0.05	1.50·10 <sup>-3</sup>	1	1.03	1.4	0.01
2	$1.2 \cdot 10^7 \pm 5.8 \cdot 10^5$	18.1 ± 0.7	172.2 ± 1.9	2.51 ± 0.08	1.48·10 <sup>-3</sup>	1	1.06	1.5	0.01
3	$1.6 \cdot 10^6 \pm 9.7 \cdot 10^4$	55.3 ± 1.0	227.3 ± 2.9	2.31 ± 0.05	1.45·10 <sup>-3</sup>	1	1.02	1.3	0.01
4	$1.5 \cdot 10^6 \pm 7.8 \cdot 10^4$	201.2 ± 7.7	242.2 ± 21.8	$2.05 \pm 0.09$	1.45·10 <sup>-3</sup>	1	1.13	0.9	0.00
isoprene acidic seeds									
5	$5.68 \cdot 10^7 \pm 1.1 \cdot 10^7$	1.5 ± 0.2	67.1 ± 0.6	4.31 ± 0.14	1.35·10 <sup>-3</sup>	1.19	1.46	3.66	0.05
6	$2.35 \cdot 10^7 \pm 9.6 \cdot 10^6$	14.1 ± 0.3	98.1 ± 0.9	4.18 ± 0.07	1.26·10 <sup>-3</sup>	1.20	1.35	3.67	0.04
7	$6.10 \cdot 10^6 \pm 2.7 \cdot 10^6$	38.1 ± 0.7	121.2 ± 1.9	4.14 ± 0.08	1.29·10 <sup>-3</sup>	1.20	1.31	3.64	0.03
8	$2.28 \cdot 10^6 \pm 4.2 \cdot 10^4$	86.9 ± 0.6	153.3 ± 1.7	3.52 ± 0.08	1.33·10 <sup>-3</sup>	1.19	1.27	2.92	0.02
9	$2.73 \cdot 10^6 \pm 8.9 \cdot 10^4$	73.6 ± 1.0	155.0 ± 2.9	3.48 ± 0.10	1.41·10 <sup>-3</sup>	1.18	1.65	2.46	0.02
10	$1.24 \cdot 10^6 \pm 4.0 \cdot 10^4$	258.7 ± 2.4	252.2 ± 6.7	$2.50 \pm 0.06$	1.30·10 <sup>-3</sup>	1.20	1.22	1.77	0.01
11	$1.30 \cdot 10^6 \pm 4.6 \cdot 10^4$	261.0 ± 2.4	262.0 ± 6.9	2.54 ± 0.11	1.30·10 <sup>-3</sup>	1.20	1.11	1.93	0.01

Table S2: Isoprene SOA yields on neutral and acidic aerosols in JPAC

### 2. SOA yield, its definition in mixtures and a perspective on OH scavenging

Here we illustrate the main controlling parameters of photochemical SOA mass formation in precursor mixtures. For clarity we will simplify our approach by assuming constant SOA yields prior to consideration of variable yields in section 3. In this discussion, as in our study, we represent the mixed state in the atmosphere by mixtures of isoprene, the major biogenic VOC<sup>7</sup> with a SOA yield of the order of a few percent (according to our observations in JPAC, Table S1 and S2), and  $\alpha$ -pinene, the most abundant monoterpene<sup>7</sup> with a SOA yield of 15% or more.

Considering  $\alpha$ -pinene in isolation being oxidised by OH, the particulate organic mass  $\Delta$ [SOA] generated in a time interval  $\Delta t$  by definition is given by consumption of  $\alpha$ -pinene during  $\Delta t$ multiplied by the  $\alpha$ -pinene SOA yield (y<sub>AP</sub>). The consumption of  $\alpha$ -pinene  $\Delta$ [AP] is time dependent and depends on the concentration of  $\alpha$ -pinene [AP]<sub>ss</sub> and the concentration of [OH]<sub>ss</sub>, which are assumed to be in a steady state indicated by the subscript ss (Eq. 1). This is the situation for many instances in the atmosphere, where sources and chemical losses balance over a time period of hours, but also in our RC.

$$\Delta[SOA]_{AP} = y_{AP} \cdot \Delta[AP]$$

$$\Delta[AP] = k_{AP} \cdot [OH]_{ss} \cdot [AP]_{ss} \cdot \Delta t$$
(1)

In the presence of isoprene a second component  $\Delta$ [SOA]<sub>Iso</sub> contributes to SOA formation (Eq 2):

$$\Delta[SOA]_{Iso} = y_{Iso} \cdot \Delta[Iso]$$
<sup>(2)</sup>

 $\Delta[Iso] = k_{Iso} \cdot [OH]_{ss} \cdot [Iso]_{ss} \cdot \Delta t$ 

. . . .

The formation of total organic mass  $\Delta$ [SOA] is generally assumed to be given by:

$$\Delta[SOA] = y_{AP} \cdot \Delta[AP] + y_{Iso} \cdot \Delta[Iso]$$

$$\Delta[SOA] = (y_{AP} \cdot k_{AP} \cdot [OH]_{ss} \cdot [AP]_{ss} + y_{Iso} \cdot k_{Iso} \cdot [OH]_{ss} \cdot [Iso]_{ss}) \cdot \Delta t$$
(3)

In Eq. 3,  $y_{AP}$  is unaffected by the presence of isoprene and vice versa  $y_{iso}$  is unaffected by the presence of  $\alpha$ -pinene. The SOA yield for a mixture of  $\alpha$ -pinene and isoprene, y<sub>mix</sub>, can then be defined by Eq. 4 using the consumption of both VOC.

$$\frac{\Delta[SOA]}{\left(k_{AP} \cdot [OH]_{ss} \cdot [AP]_{ss} + k_{Iso} \cdot [OH]_{ss} \cdot [Iso]_{ss}\right) \cdot \Delta t} = y_{mix}$$
(4)

Using the definition for  $y_{mix}$  in Eq. 4, it is obvious that it depends on the composition of the mixture. Starting from  $\alpha$ -pinene alone and then adding more and more isoprene leads to a steady decrease of y<sub>mix</sub>. The formed SOA mass is related to the total VOC consumption and the higher the contribution of isoprene consumption to the total consumption, the lower is  $y_{mix}$ . In the atmosphere, [OH]ss depends on many parameters and may not solely depend on the presence of isoprene.<sup>59,60</sup> We will differentiate two cases, either the presence of isoprene lowers the [OH]<sub>ss</sub> because it adds to the net chemical sink of OH, or [OH]ss depends more strongly on other parameters and remains about constant.

If the presence of isoprene lowers  $[OH]_{ss}$ ,  $\Delta[SOA]$  and  $y_{mix}$  will decrease in the mixture and should be lower than that for  $\alpha$ -pinene alone (for the same  $[AP]_{ss}$ ). This effect follows by

application of linear mixing rules (Eq. 5), which describes the individual contribution of each component to the total consumption, weighted by its respective yield.

$$y_{mix} = y_{AP} \cdot \frac{k_{AP} \cdot [OH]_{ss} \cdot [AP]_{ss}}{k_{AP} \cdot [OH]_{ss} \cdot [AP]_{ss} + k_{Iso} \cdot [OH]_{ss} \cdot [Iso]_{ss}}$$
(5)

$$+y_{Iso} \cdot \frac{k_{Iso} \cdot [OH]_{ss} \cdot [Iso]_{ss}}{k_{AP} \cdot [OH]_{ss} \cdot [AP]_{ss} + k_{Iso} \cdot [OH]_{ss} \cdot [Iso]_{ss}}$$

...

As stated above, we observed a yield of isoprene of roughly an order of magnitude smaller than that of  $\alpha$ -pinene in the presence of neutral preexisting aerosol or about a factor of 3 smaller with acidic aerosol (Tables S1 and S2, Figure S2, blue or red shaded ranges). The OH suppression by isoprene could lead to a reduction of SOA mass formation over certain regions of the world. Furthermore, as a result of the partitioning according to Raoult's law<sup>61-63</sup> the yield will be even smaller if less SOA is formed, which slightly enhances the OH suppression effect. (As the model results in section 8 illustrate the amount of SOA formed in real mixtures is more complex and depends on the specific concentrations of the precursors and their coupling to the oxidant fields.)

In case of constant  $[OH]_{ss}$ , *a priori* the SOA mass produced from  $\alpha$ -pinene should be the same, independent on the presence of isoprene. If isoprene is present, isoprene oxidation adds to SOA mass and the total mass of SOA would become larger despite the small yield of isoprene. If we consider the partitioning effect the yields will even increase somewhat. In case of *isoprene not affecting* [OH]<sub>ss</sub> we indeed would expect an increase of SOA mass by the presence of isoprene, as postulated in the literature (e.g.<sup>64,65</sup>).

It can readily be envisaged that apart from isoprene there are wide ranges of components of varying reactivity and SOA yields that can comprise atmospheric mixtures in different environments. This means that components contributing significantly to SOA mass will influence the OH concentrations to different degrees. This will lead to a variety of degrees to which oxidant scavenging can influence SOA mass in the atmosphere.

The oxidant effect described so far affects only  $y_{mix}$ , the yields of the individual VOC in the mixture were assumed to be constant. If we consider that the SOA yield  $y_{AP}$  itself may be OH dependent, e.g. by oxidative ageing of the vapours (e.g.<sup>31,32</sup>, references therein and section 6), the suppressing effect of isoprene will be even stronger. Regardless of whether the SOA formation is suppressed due to reduced availability of OH for reactions with the VOC, or by lower yields at lower OH concentrations, we call this phenomenon *OH scavenging* effect.

The *OH scavenging effect* due to linear mixing rules (Eq. 5) is included in the global model calculations presented in section 8 and its importance for SOA mass is evident. However linear mixing rules are not the topic of our mechanistic investigations. The focus of our mechanistic studies is the effect of isoprene on  $y_{AP}$ , i.e. we newly discovered changes of  $y_{mix}$  on top of those obvious from applying linear mixing rules. There were two effects causing the decrease of  $y_{AP}$ 

when adding isoprene: the OH dependence of  $y_{AP}$  – due to an *OH scavenging effect* – and the new *product scavenging effect*. The existence of a product scavenging effect will be derived by analysis of *SOA yields in mixtures* in the next section.



Consumption isoprene / consumption  $\alpha$ -pinene [µg]/[µg]

**Figure S2**: SOA yields of  $\alpha$ -pinene & isoprene mixtures as a function of the relative consumption (isoprene /  $\alpha$ -pinene) for neutral ammonium sulfate (blue circles) and acidic ammonium bisulfate seed aerosol (red circles). The presence of isoprene lowers the steady state concentration of OH and in both cases reduces the SOA yield of the mixture. The light blue and the orange dashes show the expectation assuming linear mixing rules and constant yields ( $y_{AP}=0.17$  for both and  $y_{1so}=0.01$  for neutral seeds and  $y_{1so}=0.04$  for acidic seeds). Blue shaded area: range of isoprene SOA yields in presence of neutral seed aerosols for pure isoprene reaction systems. Red shaded area: range of isoprene solar yields in presence of acidic aerosols for pure isoprene reaction systems. Isoprene yields are higher on acidic seed aerosols. The scattering of the data for the pure reaction systems of  $\alpha$ -pinene (circles at x = 0) and isoprene (shaded areas) is a result of experimental uncertainties as indicated by the error bars and also by variabilities in experimental reaction conditions (O<sub>3</sub>, VOC, OH production).

#### **3.** New observations: SOA yield for isoprene α-pinene mixtures

Figure S2 shows that, with increasing ratios of isoprene/ $\alpha$ -pinene consumption, i.e. larger excess of isoprene, SOA mass yield reduces by about on order of magnitude down to the yield of isoprene alone. Suppression of SOA mass and SOA mass yields by isoprene occurred in the presence of neutral as well as acidic seed aerosols (Figure S2). Herein we considered the summed consumption of both VOC to calculate  $y_{mix}$  (Eq. 4). The observed suppression effect was not fully compensated by accretion reactions of isoprene oxidation products in the particulate phase on

acidic seed particles.<sup>12,35-37</sup> In our case this led indeed to higher yields in presence of acidic aerosols and compensated for some of the suppression effects (Figure 1, and red data in Figure S2).

Simultaneous oxidation of VOC mixtures is the normal process in the atmosphere. It is not obvious how to reference the SOA mass formation to the consumption of VOC in the mixture when calculating the yield. In Figure S2 we presented the yield  $y_{mix}$  for the  $\alpha$ -pinene/isoprene mixtures using the total BVOC consumption which, in our case, is the sum of the isoprene and the  $\alpha$ -pinene consumption. The light blue markers in Figure S2 shows that we *a priori* should expect a drop of the SOA yield by reduction of [OH]<sub>ss</sub> (OH scavenging) for  $\alpha$ -pinene/isoprene mixtures, assuming linear mixing rules. The ideal mixing line calculated by applying Eq. 5 is higher than the observations indicating, that *more than simple OH scavenging* occurs and  $y_{AP}$  seems to be affected by the presence of isoprene. The same is true for the acidic seed aerosols (red markers).

In the mixtures of "low yield" SOA forming isoprene and "high yield" SOA forming  $\alpha$ -pinene studied here, it is also justified to reference the SOA yield to  $\alpha$ -pinene alone as long as  $y_{Iso} \ll$ y<sub>AP</sub>. Since this neglects the minor contribution of the isoprene SOA, it gives an upper limit for the SOA generated from  $\alpha$ -pinene at the given conditions. Referencing solely to the actual consumption of  $\alpha$ -pinene clarifies the role of  $\alpha$ -pinene in the mixture since it reflects that not only  $[OH]_{ss}$ , and thus the actual  $\alpha$ -pinene consumption was lowered by the presence of isoprene but also the SOA yield y<sub>AP</sub> itself, as described in the main manuscript (Figure 2). The result is striking. Although isoprene must have contributed somewhat to the SOA mass, at least in the acidic case, the normalized yield is always smaller than unity, which means that the production of SOA from  $\alpha$ -pinene is *less effective* in the presence of isoprene. We will show in our experiments that this effect is related to the behaviour of the recently discovered HOM and HOM dimers<sup>22,51</sup> and their removal from the pool of species contributing to SOA mass; we call this phenomenon "product scavenging". The discovery of the product scavenging effect, leading to a negative effect on y<sub>AP</sub> when adding e.g. isoprene is the core of this paper and it will challenge the concept of additive or enhanced SOA yield at constant [OH]. In the next section 4 we will describe the concepts to separate product scavenging and OH scavenging.

### 4. Experimental separation of OH scavenging and product scavenging

We have experimentally separated, isolated, and quantified the *OH scavenging* and the *product scavenging* effects. The key to this separation was the adjustment of the OH production and thus  $\alpha$ -pinene consumption was adjusted during the particular measurements to obtain the *same* OH concentration [OH]<sub>ss</sub> in presence and absence of isoprene. Such OH adjustments are a unique feature of JPAC. We performed the experiments with neutral seeds (Figure 1A) and acidic seeds (Figure S3), in order to take into account that isoprene oxidation products can undergo condensed-phase accretion reactions in acidic environments (Figure S4).<sup>35-37,66,67</sup> As neutral seeds we used ammonium sulfate particles and as acidic seeds ammonium bisulfate doped with some extra H<sub>2</sub>SO<sub>4</sub>.



**Figure S3:** *Product scavenging* and *OH scavenging* effect in the presence of acidic ammonium bisulfate seed aerosols, by isoprene (dark green circles, lower time axis) and by CO (light green triangles, upper time axis). The dark grey area shows the reaction system  $\alpha$ -pinene & OH as a reference. In the beginning of the light grey area isoprene was introduced into the chamber, in the beginning of the medium grey area OH was re-adjusted to the same value as in the dark grey period. The letters indicate periods of steady state for ozonolysis (<u>A</u>),  $\alpha$ -pinene & OH (<u>B</u>),  $\alpha$ -pinene & isoprene & isoprene & [OH] adjusted (<u>D</u>). Values in Figure 1B are taken from these periods. The organic mass was normalized to sulfate mass in order to compensate for fluctuations of the seed aerosol generation and is shown as organic to sulfate ratio (organics/SO<sub>4</sub><sup>2-</sup>, dark green circles and light green triangles).

Addition of isoprene (red triangles) lowered [OH] (black diamonds) and  $\alpha$ -pinene consumption ( $\Delta \alpha$ -pinene, blue squares), leading to reduced formation SOA mass. Re-adjusting [OH] and  $\alpha$ -pinene consumption induced enhanced SOA mass formation. This is different for the acidic seed aerosol compared to the neutral seed aerosol (Figure 1A). Later in the experiment (top axis) isoprene was removed and CO was added to the  $\alpha$ -pinene & OH system under otherwise same chamber settings. The observed organics/SO<sub>4</sub><sup>2-</sup> is shown in light green small triangles. ([OH],  $\Delta \alpha$ -pinene and  $\Delta$ CO are not shown.) Product scavenging and OH scavenging (black arows) are taking place in the presence of acidic seed aerosols as expected, since the acidity of the seed particles should not affect the gas-phase chemistry.

The red arrows are an estimate of the gain in SOA mass by isoprene that is due to condensation/acreation reactions of isoprene oxidation products on the acidic seed particles (see also Figure S4).

In Figure 1A and Figure S3 we show the AMS organic/sulfate ratio (org/SO<sub>4</sub><sup>2-</sup>, green circles) taking out trends and fluctuations of the seed aerosol generation, which were caused by limited stability of the seed aerosol production. The SOA mass yields in Figure 1B and the analysis of the isoprene contribution to SOA in Figure S4 are based on those experiments during the steady state periods B, C, and, D, marked by black horizontal lines in Figures 1A and S3.

The (wall loss corrected)  $\alpha$ -pinene SOA yield in period B is practically the same (within the experimental uncertainties) for acidic seed aerosols (20%) as for the neutral case (18%) (Figure 1B, columns B). This means, that the formation of  $\alpha$ -pinene SOA itself was not significantly affected by the acidity of the seed particles.



**Figure S4:** Isoprene oxidation products contribute to organic mass in the presence of acidic seed particles.  $C_2H_5O^+$  (green) served as marker ion for the -pinene contribution, whereas  $CH_3O^+$  (brown) and  $C_5H_6O^+$  (beige) served as marker ions for the isoprene oxidation products. All marker ion signals were normalized to  $C_2H_5O^+$  during respective phase B. Note that the mass contribution of the individual marker ions to total organic mass is only of the order of percent. In the presence of **neutral seeds** (left side)  $C_2H_5O^+$  followed the concentration of the total organic mass closely. Note that  $\alpha$ -pinene oxidation products contribute somewhat to the ions  $CH_3O^+$  (brown) and  $C_5H_6O^+$ (beige), but the two ions vary proportional to the  $C_2H_5O^+$  ion. In the presence of **acidic seeds** (right side) the ions  $CH_3O^+$  and  $C_5H_6O^+$  showed the same low contribution in the absence of isoprene (A, B) as in the neutral case. However, both marker ions increased strongly when isoprene was added to the reaction chamber (C). They increased further when [OH] was re-adjusted (D), because of the fast reaction of isoprene with OH radicals. Clearly, isoprene oxidation products also contribute somewhat to the  $C_2H_5O^+$  marker ion.

Addition of isoprene (red triangles) to the evolved  $\alpha$ -pinene & OH system dropped [OH]<sub>ss</sub> to about 1/3 in period C (black diamonds in light grey area). The reduction of [OH] in period C has two effects: it reduced the  $\alpha$ -pinene consumption (blue squares) thus the production of SOA mass. Moreover, the *SOA yield is lower* at lower OH due the product scavenging effect induced by the presence of isoprene (and somewhat due to OH dependence of the SOA yield in general<sup>31,32</sup>). The suppression of SOA mass is more distinct in presence of neutral aerosol (Figure 1A) than in presence of acidic aerosol (Figure S3). But also the *SOA yields* are reduced in both cases, by about 40% in the neutral case and by about 1/3 in the acidic case (second columns in Figure 1B). This suppression of the SOA yield we attribute to the sum of *product scavenging* and *OH scavenging* effects.

In period D (middle grey area)  $[OH]_{ss}$  and thus the  $\alpha$ -pinene consumption were re-adjusted in the presence of isoprene to the same values as observed for the  $\alpha$ -pinene only system. As a consequence the effect of OH scavenging (marked in orange in Figures 1A and S3) is compensated. The effect is striking in the presence of neutral seed aerosol: the SOA mass remains reduced (Figure 1A) and the SOA yield is distinctively smaller when isoprene is present (Figure 1B, column D). This difference we attribute to the effect of product scavenging (marked in red in Figure 1A). As we will show in section 6, product scavenging is due to interaction of  $\alpha$ -pinene peroxy and isoprene-induced peroxy radicals in the HOM formation process.

In the presence of acidic aerosol, the SOA mass increased after re-adjustment, however the SOA yield still remains lower. Since the acidity of the aerosols will hardly influence the gas-phase chemistry, both scavenging effects were apparently masked by isoprene oxidation products contributing to SOA mass on acidic seeds (red arrows in Figure S3). Indeed, while in case of a neutral seed aerosol we found no significant influence of SOA composition by the presence of isoprene, we directly observed the isoprene markers by aerosol mass spectrometry on the acidic seed aerosol (Figure S4) likely arising from condensed phase accretion reactions.<sup>35-37,66,67</sup> The suppression of  $\alpha$ -pinene SOA is compensated by some isoprene SOA (iSOA). Nevertheless the suppression of total SOA *yield* was still recognizable in the presence of acidic seeds (Figure 1B) and even more so in Figure 2. Note that in both OH adjustment experiments (Figure 1A and Figure S3) the consumption of  $\alpha$ -pinene and isoprene in terms of mixing ratio are quite similar. This choice was determined by the experimental boundary conditions for such complex experiments. This means that the ratio of  $\Delta$ isoprene/ $\Delta \alpha$ -pinene in units of mass concentration is about  $\frac{1}{2}$  only, thus on the very left side in Figure 2. Insofar, the product scavenging effect is expected to be much larger at higher  $\Delta$ isoprene/ $\Delta \alpha$ -pinene.

The iSOA contribution can be estimated by comparison with the SOA mass formation when isoprene is replaced by CO at otherwise same conditions (Figure S3, light green trace). In contrast to isoprene oxidation products, the CO oxidation product  $CO_2$  cannot contribute to SOA formation. In presence of CO the OH scavenging effect and the product scavenging effect after re-adjustment of  $[OH]_{ss}$  in presence of acidic aerosols in Figure S3 were strikingly similar to the effect of isoprene in presence of neutral aerosols in Figure 1A.

The strength of the compensating effect of accretion reactions of isoprene oxidation products, as indicated by the red arrows in Figure S3, is of course larger at higher  $[OH]_{ss}$ , thus higher isoprene consumption. A difference between isoprene and CO is that isoprene raised the level of organic peroxy radicals with  $\leq$  5 carbon atoms (and HO<sub>2</sub> radicals), while CO raised only the level of HO<sub>2</sub> radicals. The interaction of both types of peroxy radicals with  $\alpha$ -pinene peroxy radicals in HOM formation are the core of the product scavenging effect.

We conclude that the *product scavenging* effect is also active in presence of acidic seed aerosols, as the gas-phase peroxy chemistry should not be affected by the acidity of the seed particles, however the effect is masked / compensated by accretion reactions of isoprene oxidation products. As we document in the main manuscript (Figure 4) and in section 5, the findings shown here for  $\alpha$ -pinene & isoprene and  $\alpha$ -pinene & CO demonstrate a general behavior. In further experiments we showed that CH<sub>4</sub> also suppresses SOA yields of  $\alpha$ -pinene, and that isoprene also suppresses the SOA yield of  $\beta$ -pinene.



**Figure S5:** Product scavenging and OH scavenging in the reaction system  $\alpha$ -pinene & isoprene & OH. The actual SOA yield, calculated as actual organic mass / actual  $\alpha$ -pinene consumption, can serve as diagnosis of the product scavenging effect. The actual yield decreases by more than 50%, when isoprene is added to the reaction system, mainly because of product scavenging. By referring to the actual  $\alpha$ -pinene consumption the OH scavenging through the linear mixing effect of is taken out. The grey-shaded area shows the effect at 1:1  $\alpha$ -pinene/isoprene ratio at chamber inlet.

### 5. Generality of OH and product scavenging and suppression of SOA yields.

Product scavenging is not only operative in the  $\alpha$ -pinene & isoprene & OH system. We illustrated that already for  $\alpha$ -pinene & CO & OH system in presence of neutral aerosols and acidic aerosols (Figures 4 and S3). As we showed in Figures 1B and 2, a necessary strong indicator for product

scavenging is a lower *actual SOA yield*. If the OH cannot be adjusted (like in Figure 1A), inspection of the actual SOA yield in presence and absence of the scavenger can still provide a diagnostic for product scavenging, since the yield is normalized to the actual precursors consumption thus takes out the part of the simple OH scavenging effect related to the linear mixing rules (section 2). The example for the  $\alpha$ -pinene & isoprene & OH system is given in Figure S5. In the same sense product scavenging is also observed in the  $\beta$ -pinene & isoprene & OH system (Figure S6). Here the actual yield of  $\beta$ -pinene SOA is suppressed by about 40%, clearly indicating that product scavenging by isoprene is not limited to  $\alpha$ -pinene.



Figure S6: Product scavenging and OH scavenging effect in reaction system  $\beta$ -pinene & isoprene & OH. The actual SOA yield, calculated as actual organic mass / actual  $\beta$ -pinene consumption, decreases by 40%, when isoprene is added to the reaction system.

Also in binary mixtures of  $\alpha$ -pinene and compounds without SOA forming potential, like CO and CH<sub>4</sub>, a decrease of the actual  $\alpha$ -pinene SOA yield was observed, thus product scavenging can be diagnosed. In **Figure 4**, the additions of CO (10 ppm, 57 ppm) to the  $\alpha$ -pinene & OH system suppresses the total HOM by a factor 4-5 and the dimer fraction by more than a factor of 2 (**Figure 4A**). The actual SOA yield of  $\alpha$ -pinene was reduced by more than 60% in the presence of 40 ppm CO.

The most abundant organic peroxy radical in the atmosphere is  $CH_3O_2$ , which is formed in the atmospheric degradation of methane  $CH_4$  by OH. Mixing  $\alpha$ -pinene and  $CH_4$  in presence of acidic seed aerosols also leads to suppression of the  $\alpha$ -pinene SOA yield (Figure S7). Note: the conditions in JPAC were forced to yield a significant consumption of methane in order to generate  $CH_3O_2$  radicals. To estimate the possible effect of  $CH_4$  on SOA formation under

atmospheric conditions we corrected for the too high  $CH_3O_2$  radicals produced in our chamber. We use  $\alpha$ -pinene as a surrogate of all MT, and the OH reactivities of  $CH_4$  and  $\alpha$ -pinene as estimate of the ratio of  $CH_3O_2$  and  $\alpha$ -pinene peroxy radicals ( $R_{CH4}/R_{MT}$ ). Summer monoterpene concentrations at the SMEAR station in Hyytiälä are typically several 100 ppt<sup>68</sup> and  $CH_4$  is around 1.8 ppm;  $R_{CH4}/R_{MT}$  in Hyytiälä is about 0.6 assuming 300 ppt MT. In the experiment shown in Figure S7 the ratio of  $CH_4$  reactivity /  $\alpha$ -pinene reactivity was ~ 2 and the yield of  $\alpha$ -pinene was suppressed by about 50 %. If we choose the simplest approach, i.e. to scale the suppression of SOA formation with  $R_{CH4}/R_{MT}$  (= ratio of consumption), we estimate an suppression of the order of 15 %. If the  $CH_4$  chemical system behaves in a similar manner to the isoprene system than we would expect a suppression of 16% from the parametrisation as given in Figure 2. Furthermore, at the relative constant ambient  $CH_4$  concentrations, the relative impact of  $CH_4$  should increase with decreasing monoterpene concentrations.



**Figure S7:** Product scavenging effect in reaction system  $\alpha$  -pinene & CH<sub>4</sub> & OH. The actual SOA yield, calculated as actual organic mass / actual  $\alpha$  -pinene consumption, drops, when CH<sub>4</sub> is added to the reaction system. CH<sub>4</sub> concentrations were calculated from known inlet concentration, the flow rate through the RC and the reaction rate of CH<sub>4</sub> with OH.

Given the generality of product scavenging, it is obvious that the SOA mass formed from a mixture cannot be approximated linearly. Calculating the SOA mass formed by oxidation of individual compounds from their individual yields and their consumption and then adding up these SOA masses will overestimate the total SOA formation. The basic mechanisms identified here show that - due to basic photochemical processes - the SOA yield of an individual compound also depends on other molecules in the respective environment.

### 6. Gas-Phase HOM Chemistry: Dimer Suppression

Peroxy radicals are key players in atmospheric oxidation of organic compounds. They are formed via H-abstraction by OH or addition of OH to double bonds. During ozonolysis, peroxy radicals are also formed via the vinylhydroperoxide path. In competition with termination reactions, peroxy radicals can undergo intramolecular H-shifts forming a hydroperoxide group and a carbon centered radical.<sup>45,69,70</sup> The latter rapidly adds air oxygen reforming the peroxy functionality. The sequence of H-shifts and O<sub>2</sub> addition is called autoxidation<sup>71</sup> and can lead to very fast formation of highly oxygenated multifunctional peroxy radicals (HOM-RO<sub>2</sub>) with O/C up to one or even higher. HOM-RO<sub>2</sub> are terminated like other peroxy radicals<sup>45</sup> and the interplay of autoxidation and termination reactions results in stable highly oxygenated multifunctional molecules (HOM<sup>22,45,52,70</sup>). In our experiments at low NO concentrations HOM-RO<sub>2</sub> are mainly terminated by other peroxy radicals, including HO<sub>2</sub>. HOM are compounds of low or extremely low volatility (LVOC or ELVOC)<sup>22,39,72</sup> and we will show that the reduction of SOA yields due to the product scavenging effect are related to changes in HOM.

In order to understand the product scavenging effect on molecular level it is important to note that in reactions between HOM-RO<sub>2</sub> also HOM-dimers are formed, e.g.  $C_{17}$ - $C_{20}$ -HOM in the case of  $\alpha$ -pinene (Figure S8)<sup>22,38</sup>. The O/C ratios of HOM dimers are typically lower than those of HOM monomers, and, as shown for cyclopentene and cyclohexene, dimers involve also the most abundant primary peroxy radicals<sup>45</sup>. The exact mechanism of the self-dimerization is yet not clear, but rates for dimer formation are high for functionalized RO<sub>2</sub> radicals<sup>38</sup>, sufficiently high to compete with termination reactions with RO<sub>2</sub> and HO<sub>2</sub>. From their structure and their O/C ratios dimers are organic compounds with extreme low volatility (ELVOC) <sup>38,39,45,70,72</sup> and HOM-monomers and HOM-dimers together can dominate SOA formation, up to 50%-100% in early phases of SOA formation.<sup>22</sup>

We studied the HOM *gas-phase* chemistry for  $\alpha$ -pinene and  $\alpha$ -pinene/isoprene mixtures by Chemical Ionization Time of flight Mass Spectrometry and could observe directly the suppression of  $\alpha$ -pinene HOM-dimers in the presence of isoprene (see Figure 3A). This effect of isoprene becomes clear by comparing the HOM distribution in monomers and dimers at the same  $\alpha$ -pinene turnover in Figure 3B, with the [OH] tuned by either adding different amounts of isoprene (red) or by modifying the O<sub>3</sub> photolysis rate J(O<sup>1</sup>D) (blue). We grouped HOM-monomers and HOM-dimers using the center of the mass spectrum envelope at m/z = 370 Th as separation criterion, and took the sum over all m/z as HOM-total. For easier comparison we normalized the data for the observations at the highest turnover where [isoprene] approached zero.


**Figure S8:** Relative contribution of HOM monomers,  $\alpha$ -pinene derived  $C_{17}$ - $C_{20}$  dimers and potentially mixed  $C_{11}$ - $C_{15}$  dimers isoprene/ $\alpha$ -pinene with  $C_{15}$  separated as lead mixed dimer before isoprene addition (left) and at maximum isoprene concentration (right).  $C_{11}$ - $C_{15}$  dimers were also observed in the  $\alpha$ -pinene only system, but only as small fraction. The drop of the  $C_{17}$ - $C_{20}$  fraction is due to both OH and product scavenging. The fraction of  $C_{11}$ - $C_{14}$  dimers and the lead  $C_{15}$  dimer increase somewhat in the presence of isoprene indicating that indeed mixed isoprene/ $\alpha$ -pinene dimers are formed, but not in large amounts. The data were normalized by 344 cts (left) and 151 cts (right).

The total HOM concentration decreases more strongly when [OH] is decreased by increasing isoprene concentrations, than by decreasing the photolytic production of OH (as described in the main manuscript, Figure 3B, red and blue circles). This is mainly due to the decrease of the HOM dimer concentration, clearly decreasing more strongly with increasing isoprene than with decreasing  $J(O^{1}D)$  (red and blue squares, respectively). Based on the molecular formulas assigned to each m/z in high resolution mass spectra, we weighted the signal for each compound by the molecular mass and summed up the so derived "mass concentrations" for all monomers  $(C \le 10)$  and all dimers (C > 10). A peak list of the attributed molecular formulas for the most prominent signals is given in Table S3a andb. For an  $\alpha$ -pinene turnover of  $5 \times 10^7$  cm<sup>-3</sup> s<sup>-1</sup> (middle arrow in Figure 3B) we estimated the suppression of the HOM-dimers (dark green bars, Figure 3C). For that we scaled the mass concentrations from the  $\alpha$ -pinene J(O<sup>1</sup>D) experiment, which was performed at a lower  $\alpha$ -pinene inlet mixing ratio (10 ppb vs. 25 ppb) by a factor 2.3, to match the same (initial) conditions as for the  $\alpha$ -pinene-only reference experiment for the isoprene series and then interpolated the observations at  $4.3 \cdot 10^7$  cm<sup>-3</sup> s<sup>-1</sup> and  $5.7 \cdot 10^7$  cm<sup>-3</sup> s<sup>-1</sup> to  $5.0 \cdot 10^7$  cm<sup>-3</sup> s<sup>-1</sup> as indicated in Figure 3C. We estimate a drop by 33% of the total HOM mass of which 26% is due to reduced HOM-dimer concentrations and the other 7% due to HOM-monomers. Since we compare values at the same  $\alpha$ -pinene turnover this reflects indeed the effect of product scavenging.

Assuming that SOA is predominantly formed from HOM and that HOM-dimers are effectively non-volatile and will fully contribute to SOA mass, the 27% mass suppression of HOM dimers explains most of the overall reduction of SOA mass of about 35%, due to the product scavenging effect in Figure 1A. Note again that HOM are responsible for 50-100% of the SOA mass under these conditions and that the reduction predicted from the suppression of dimers fits the experimentally determined reduction of SOA mass quite well.

α-Pinene					α-Pinene + isoprene								
Formula			Exact mass [m/z]	HOM [Da]	error [ppm]	rel intensity [%]	Formula			Exact mass [m/z]	HOM [Da]	error [ppm]	rel intensity [%]
C5	C5 H	5 O6	224.005	162.016	2.2	0.73	C5	C5 H6	07	240.000	178.011	-1.3	0.79
	C5 H	7 06	225.013	163.024	-1.4	0.21		C5 H8	08	258.010	196.022	-3.5	1.5
	C5 H	5 07	238.992	177.004	-12.7	0.38		C5 H10	08	260.026	198.038	-10.9	1.61
	C5 H	5 07	240.000	178.011	-1.3	0.31		C5 H9	09	275.013	213.025	2.6	0.68
	C5 H	7 07	241.008	179.019	-5.2	0.31		C5 H10	09	276.021	214.032	-2.9	0.87
C10	C10 H1	6 O6	294.083	232.095	4.7	1.06	C10	C10 H16	O6	294.083	232.095	10.5	0.54
	C10 H1	4 07	308.062	246.074	1.7	0.82		C10 H14	07	308.062	246.074	-3.9	1.33
	C10 H1	6 07	310.078	248.090	-3.6	9.58		C10 H16	07	310.078	248.090	-7.6	6.02
	C10 H1	4 08	324.057	262.069	5.8	1.53		C10 H14	08	324.057	262.069	5.2	1.26
	C10 H1	6 08	326.073	264.085	-6.1	4.49		C10 H16	08	326.073	264.085	-13.0	1.5
	C10 H1	4 09	340.052	278.064	5.9	1.05		C10 H14	09	340.052	278.064	13.3	1.18
	C10 H1	6 09	342.068	280.079	-9.3	1.85		C10 H16	09	342.068	280.079	-14.0	1.78
	C10 H1	4 010	356.047	294.059	13.1	0.78		C10 H14	O10	356.047	294.059	13.1	0.74
	C10 H1	6 O10	358.063	296.074	-4.4	0.81		C10 H16	010	358.063	296.074	-4.4	0.91
	C10 H1	5 011	373.050	311.061	-10.0	0.86		C10 H15	O7 HNO3'NO	3- 372.066	247.082	6.0	0.51
	C10 H1	6 07 HNO3*NO	3- 373.074	248.090	-7.8	2.58		C10 H15	011	373.050	311.061	-10.0	0.76
	C10 H1	6 011	374.058	312.069	3.1	0.66		C10 H16	O7 HNO3*NO	3- 373.074	248.090	-7.8	1.59
	C10 H1	4 08 HNO3"NO	3- 387.053	262.069	-4.6	1.04		C10 H14	O8 HNO3'NO	3- 387.053	262.069	-4.6	0.91
	C10 H1	6 08 HNO3'NO	3- 389.069	264.085	-13.7	1.14		C10 H16	O8 HNO3*NO	3- 389.069	264.085	-13.7	0.52
C15	C15 H2	2 09	408.115	346.126	7.3	0.26	C15	C15 H24	010	426.125	364,137	-9.9	0.42
	C15 H2	2 010	424.110	362.121	-8.6	0.25		C15 H26	010	428.141	366.153	-2.7	0.49
	C15 H2	2 011	440.105	378.116	13.8	0.6		C15 H24	011	442.120	380.132	-10.1	0.54
	C15 H2	2 012	456.099	394.111	-6.7	0.25		C15 H24	012	458.115	396.127	-1.9	0.43
	C15 H2	4 012	458.115	396.127	-1.9	0.16		C15 H26	013	476.126	414.137	-11.1	0.33
C20	C20 H3		476.177	414.189	-7.0	0.82	C20	C20 H34		464.214	402.225	-3.9	0.15
	C20 H3		492.172	430.184	-9.2	0.87		C20 H32		478.193	416.205	9.3	0.14
	C20 H3		494.188	432.200	-1.9	0.45		C20 H32		494.188	432.200	1.3	0.15
	C20 H3 C20 H3		508.167 510.183	446.179 448.194	-7.6	1.52		C20 H34 C20 H30		496.204 508.167	434.215 446.179	15.6	0.15
	C20 H3		524.162	462.174	-8.9	0.93		C20 H30		510.183	448,194	-1.8	0.31
	C20 H3		526.178	464,189	10.0	1.09		C20 H32		524.162	462.174	-8.9	0.17
	C20 H2		539.149	477.161	3.2	0.31		C20 H32		526.178	464,189	10.0	0.4
	C20 H3	0 013	540.157	478.169	-7.4	0.99		C20 H30		540.157	478.169	-7.4	0.21
	C20 H3	0 014	556.152	494,164	-8.8	0.49		C20 H32	013	542.173	480.184	11.0	0.16

Table S3 Peak lists for α-pinene and α-pinene & isoprene mixtures

The interaction of  $\alpha$ -pinene HOM peroxy radicals with isoprene peroxy radicals, does not lead to significant contributions to mixed  $\alpha$ -pinene-isoprene dimers. In Figure S8 we compare the sum of HOM-monomer concentrations with several HOM dimer-concentrations before and at the maximum of isoprene addition with  $\alpha$ -pinene input (25 ppb) held constant. We chose C<sub>17</sub>-C<sub>20</sub> compounds (dark green) as lead class of  $\alpha$ -pinene derived dimers, and C<sub>11</sub>-C<sub>15</sub> compounds (reddish) as lead class of potential mixed  $\alpha$ -pinene/isoprene dimers. We also show C<sub>15</sub>-HOM (red) as marker for direct C<sub>10</sub>-peroxy + C<sub>5</sub>-peroxy radical recombination. First we note that C<sub>11</sub>-C<sub>15</sub> dimers are also formed by  $\alpha$ -pinene and C<sub>15</sub>-HOM provides the major contribution to the C<sub>11</sub>-C<sub>15</sub> class. In this case C<sub>11</sub>-C<sub>15</sub> dimers must arise from fragmented  $\alpha$ -pinene oxidation products. The concentration of C<sub>17</sub>-C<sub>20</sub> dimers (dark green) is about five times higher than C<sub>11</sub>-C<sub>15</sub> dimers (reddish). C<sub>17</sub>-C<sub>20</sub> dimers are  $\approx$ 35% of the total HOM in absence of isoprene. When isoprene is

maximal, HOM monomers (light green) drop by 40%, mainly due to the OH scavenging effect by isoprene, however  $C_{17}$ - $C_{20}$  dimers drop by  $\approx$ 90% due to both OH and product scavenging effect.  $C_{11}$ - $C_{15}$  dimers and  $C_{15}$ -HOM marker are still lower than in absence of isoprene because the isoprene induced drop in [OH] over-compensates the formation of isoprene derived  $C_{11}$ - $C_{15}$  dimers and the  $C_{15}$ -HOM marker. The relative increase of  $C_{11}$ - $C_{15}$  dimer fraction offsets only very little of the product scavenging effect in accordance with the observation in Figure 2A, where only weak signals were recognizable in the  $C_{15}$ -HOM *m/z* range.

We conclude that the product scavenging effect in the presence of isoprene is due to additional termination reactions of  $\alpha$ -pinene HOM-RO<sub>2</sub> with isoprene RO<sub>2</sub> and isoprene related increased HO<sub>2</sub>. This clearly reduces the concentration of  $\alpha$ -pinene dimers and explains already a major portion (4/5) of the SOA mass reduction. As indicated in the mass spectrum in Figure 2A presence of isoprene shifted in addition the HOM monomers to smaller masses, thus to higher vapour pressures. Both contributions led to less HOM with extreme low vapour pressures and reduced SOA mass. Our findings are in accordance with the suggestions that HOM-dimers and only a fraction of HOM monomers are ELVOC.<sup>25,64</sup>

It is interesting to note that the overall HOM signal, comprising monomers and dimers, is increasing nearly linearly with the  $\alpha$ -pinene turnover on a logarithmic scale, indicating non-linear behavior (Figure 3B). This is independent on the OH concentration being varied by different isoprene additions or by varying J(O<sup>1</sup>D). One reason is that HOM themselves are likely formed by a combination of autoxidation and sequential oxidation. The observed non-linearity with OH suggest that at least one extra oxidation step is involved of the formation of a portion of the HOM. Indeed, mass spectra of HOM derived from oxidation of pinonaldhyde by OH look very similar to those derived from a-pinene in the same way, and both are distinct from mass spectra derived from  $\alpha$ -pinene ozonolysis. Since HOM contribute significantly to SOA, we conclude that the non-linear dependence of HOM formation on OH can explain parts of the OH dependence of the SOA yields observed for  $\alpha$ -pinene and  $\beta$ -pinene (e.g.<sup>31,32</sup>).

Note HOM are very likely a mixture of LVOC and ELVOC from primary and secondary oxidation. A certain fraction of HOM are ELVOC (10-20%)<sup>39</sup> and the condensed LVOC and ELVOC provide an organic matrix for dissolution of semi-volatiles into particles. Although HOM will contribute large portions to SOA mass, this does not exclude significant contributions by products arising from classical ageing, i.e. sequential oxidation by OH<sup>e.g.2</sup>.

#### 7. Model study of isoprene chemistry under conditions prevailing in JPAC

The SOA yield from isoprene has been treated in numerous publications and estimates range from a few percent up to 30% illustrating the complexity of the chemistry including heterogeneous and in parts acid catalyzed condensed phase processes.<sup>10,12,73-78</sup> The yields of isoprene SOA (iSOA) in our experiments are on the low side of observations. Studies have shown that iSOA yields in chamber studies are sensitive to the oxidation conditions, e.g. on [HO<sub>2</sub>] and [RO<sub>2</sub>].<sup>10,74</sup> In the following we will present results from model calculations that show

that the key SOA precursor and  $HO_2$  concentrations for our experimental conditions in JPAC should be either comparable or even higher than in the atmosphere. For that we will utilize box model calculations under the boundary conditions of a perfectly stirred continuous tank reactor (CSTR) for JPAC.



**Figure S9:** Exemplary reaction scheme for oxidation of isoprene by OH leading to iSOA precursors (compare<sup>74,79,80</sup>). Two types of iSOA precursor species are formed via ISOPOOH: IEPOX (acidic aerosols) and ISOP(OOH)<sub>2</sub> (neutral aerosols). Note: the structures depicted are just examples for a set of stereoisomers.

Figure S9 summarizes a part of the isoprene oxidation mechanism that we would like to address: isoprene is oxidized by OH addition to one of the isoprene double bonds resulting in the formation of several isomeric isoprene hydroxyl peroxy radicals OH-ISOP-O<sub>2</sub>. These either react in the usual way with NO, HO<sub>2</sub>, and other peroxy radicals (RO<sub>2</sub>) or rearrange to form hydroperoxy aldehydes (HPALD) or HOM-like compounds by autoxidation.<sup>10,41,74,79-82</sup> At low NO<sub>X</sub> in non-polluted areas, corresponding to the regimes that were addressed in our study, termination by HO<sub>2</sub> forming hydroxyl hydroperoxides (ISOPOOH) is a major pathway.

Reaction of OH with ISOPOOH occurs predominantly by addition to the remaining double bond, which has two pathways (Figure S9).<sup>10,76,79,83</sup> The major pathway leads to formation of isoprene epoxydiols (IEPOX) with regeneration of OH (70%-80%), while the minor pathway, after O<sub>2</sub> addition, leads to a dihydroxy hydroperoxy peroxy radical (ISOP(OOH)O<sub>2</sub>,  $10\%^{74,79,83}$ ). This

complex peroxy radical can subsequently undergo bimolecular reactions with HO<sub>2</sub>, NO, or RO<sub>2</sub>, leading to the respective products, or undergo autoxidation via isomerisation. A significant product is the compound with O/C = 6/5 and H/C = 12/5, formed from the termination reaction with HO<sub>2</sub> (Figure S9), and hereafter referred to as ISOP(OOH)<sub>2</sub>. IEPOX form significant amount of SOA by condensed phase chemistry on acidic aerosols but are not so important in the presence of neutral aerosols. Recent experiments starting from ISOPOOH indicate a significant build-up of SOA material in presence of neutral particles based on the dihydroxy-dihydroperoxy path and ISOP(OOH)<sub>2</sub>.<sup>10,66,74,76,79</sup>

In order to get a hold of the peroxy radicals concentrations  $[HO_2]$  and  $[RO_2]$  as well as on the concentrations of ISOPOOH and the IEPOX SOA precursors in the gas-phase, we applied the MCM v3.3.1 mechanism adapted to JPAC which included an updated isoprene mechanism<sup>80</sup>. We deduced also ISOP(OOH)<sub>2</sub> and HOM, which are not included in the updated MCM v3.3.1 for isoprene, from the model calculations.

We conducted free running forward calculations varying the isoprene input concentrations over our experimental range. The intensity of the TUV lamp (254nm), thus primary ozone photolysis, was adjusted by less than 5% to reproduce the observed  $[O_3]_{ss}$  in the RC. Residence time was kept fixed at 50 min for all model runs. Model calculations were performed using the model environment EASY which is an interface for the FACSIMILE solver for differential equations.<sup>84</sup>

Experiments with isoprene for determination of the iSOA yields were performed at two different  $O_3$  inlet concentrations ( $[O_3]_{in}$ ) of 110 ppb and 55 ppb in presence of neutral and acidic seeds, respectively, but otherwise at similar boundary conditions.  $[O_3]_{in}$  is the only difference in the boundary conditions from the view point of the gas-phase chemistry and thus stand also for the two experimental cases neutral and acidic seeds. In addition we run an "atmospheric" case, simulating "typical" ambient actinic flux, OH and isoprene concentrations (see below).

In the model runs, the isoprene inflow was increased stepwise and for each increment the reactions system was calculated into a new steady state (model output after 6 h reaction time at 50 min residence time). The steady state model outputs were compared to the experimental observations. The observables which we compared to the model were isoprene ( $[C_5H_8]$ ) in the chamber, isoprene consumption (inlet concentration -  $[C_5H_8]$ ), ozone and OH. The latter was determined from the isoprene consumption.

Figure S10A and S10B show good agreement between the model and the measurements especially considering the minor adjustments applied. Deviations between the model and observation depend on uncertainties in the detailed flows delivering  $O_3$ ,  $H_2O$  and isoprene to the chamber. The comparison is less convincing at the very high inlet isoprene concentrations. The model reproduces [OH] well within the experimental error of a factor of two. The other observables were satisfactorily reproduced by the model: <10% deviation for isoprene steady state concentration, and < 5% for  $O_3$ . We therefore feel confident to use the model results for [HO<sub>2</sub>], [RO<sub>2</sub>], IEPOX, and ISOPOOH to discuss the extrapolation of our JPAC results to atmospheric conditions.



**Figure S10:** Comparison of model and observation for the experiments wherein the iSOA yields were determined on neutral (panel a,  $[O_3]_{in} = 110$  ppb) and acidic aerosol (panel b  $[O_3]_{in} = 55$  ppb). The steady state concentrations of OH, isoprene and O<sub>3</sub> are shown as a function of the isoprene inflow  $[C_5H_8]_{in}$  as well as the isoprene consumption which is the difference between inlet and outlet of the reaction chamber. Each point is one steady state experiment for the given isoprene mixing ratio in the inflow.

In order to mimic the atmospheric situation in a simple fashion, we run the model for JPAC with fixed [OH] of  $5 \times 10^6$  cm<sup>-3</sup>, ozone as in the acidic seed case ([O<sub>3</sub>]<sub>in</sub> = 55 ppb) and at isoprene steady state concentrations in a range from 1 - 15 ppb ([C<sub>5</sub>H<sub>8</sub>]<sub>in</sub> = 2.5 - 35 ppb). The photolysis frequencies were set to 50% of noon values at the equator. The results for the so defined atmospheric case will then be compared to the corresponding model results for the experimental neutral and the acidic case.

#### Gas-phase concentration of key species

Under the boundary conditions where the yields for iSOA were determined  $[HO_2]$  was about  $0.8 \cdot 10^{10}$  and  $1.4 \cdot 10^{10}$  cm<sup>-3</sup> for acidic and neutral seed simulation, respectively (Figure S11 lower panel, blue diamonds and blue triangles), thus always higher than the  $[HO_2]$  of  $3-7 \cdot 10^9$  cm<sup>-3</sup> for the simulation of atmospheric condition (blue open circles).  $[RO_2]$  (green) was less than a factor of two higher and less than a factor 3 higher for acidic (diamonds) and neutral case (triangles), respectively. The OH production is much stronger in JPAC compared to the atmosphere leading to higher OH concentrations when low concentrations of isoprene are fed to the RC. However, the input of isoprene concentrations > 100 ppb brings [OH] in the range of atmospheric concentrations (Figure S11, upper panel).



**Figure S11:** OH (orange, top), HO<sub>2</sub> (blue), RO<sub>2</sub> (green), HO<sub>2</sub>/RO<sub>2</sub> (black, right axis) for gas-phase chemistry simulated for the JPAC conditions during the iSOA yield experiments with acidic seeds (diamonds, inlet 55 ppb O<sub>3</sub>) and neutral seeds (triangles, inlet 110 ppb O<sub>3</sub>). Isoprene input was varied from 25 to 350 ppb. Open circles show a simulation with OH =  $5 \times 10^6$  cm<sup>-3</sup>, 55 ppb O<sub>3</sub> at inlet, and isoprene input ranging from 2.5 to 35 ppb (photolysis frequencies were set to 50% of the equator noon actinic flux).

Isomers of ISOPOOH are the pivotal compounds for the formation of IEPOX,  $ISOP(OOH)_2$  and HOM which control iSOA formation. In the range of isoprene turnover where the iSOA yields were determined, ISOPOOH in the chamber was either about the same or up to factors of 4 or 6 higher than the maximum in the atmospheric case. Consequently, ISOPOOH concentrations were sufficiently large in the iSOA yield experiments and regarding ISOPOOH we don't expect a large bias to low iSOA yields by specific JPAC conditions.

Reasonable concentration levels of ISOPOOH and OH also guarantee reasonably high production of IEPOX, the drivers of the higher isoprene iSOA yields on acidic seed aerosols. IEPOX ranges from  $6 \times 10^{10}$  cm<sup>-3</sup> to  $1.4 \times 10^{11}$  cm<sup>-3</sup>, which is the same as or up to a factor of two higher compared to the atmospheric simulation. In presence of neutral seeds mainly ISOP(OOH)2 and isoprene HOM should contribute to iSOA, also formed from ISOPOOH via ISOP(OOH)O<sub>2</sub>.<sup>10,74,76,83</sup> We considered the minor OH abstraction pathway (not included in MCM v3.3.1) with a branching ratio of  $10\%^{79}$  (Figure S9). Applying [HO<sub>2</sub>], [RO<sub>2</sub>], [NO] derived in the model calculations, we calculated the branching ratio for the reactions of ISOP(OOH)O<sub>2</sub> (Figure S9). We find that the major portion (85%) leads to the functionalized epoxide IEPOXOOH,  $\approx 10\%$  to ISOP(OOH)<sub>2</sub>, and  $\approx 5\%$  into the permutation reactions for the conditions of the neutral seeds. This compares to 91%, 6%, and 3%, respectively, for the atmospheric simulation. In contrast to ISOP(OOH)<sub>2</sub> the vapour pressure of IEPOXOOH is too high to condense on neutral aerosols<sup>10,74</sup>, but it will likely undergo condensed phase reaction in acidic seeds, as other IEPOX. ISOP(OOH)<sub>2</sub> molar yields are estimated to 1% under JPAC conditions compared to 0.5% for the atmospheric simulation.

As an alternative to ISOP(OOH)<sub>2</sub> we calculated an "MCM v3.3.1 surrogate" of the total isoprene HOM concentration, for which we summed up all model compounds with  $O/C \ge 6/5$  in the reaction scheme. These HOM predicted by MCM v3.3.1 were maximal  $\approx 1 \times 10^9$  cm<sup>-3</sup> for the atmospheric case, and maximal  $\approx 7 \times 10^9$  cm<sup>-3</sup> for the experiment conditions with neutral seeds. The predicted HOM concentrations compare well with the estimated values for the ISOP(OOH)<sub>2</sub> channel of about 1-2.5x10<sup>9</sup> cm<sup>-3</sup> for the atmospheric case and of  $\approx 0.5$ -1.5 x 10<sup>10</sup> cm<sup>-3</sup> for the neutral seed case.

In summary, iSOA yields in JPAC are not biased to too low values because of too low concentrations of the major iSOA precursors for neutral (ISOP(OOH)<sub>2</sub>, HOM) or acidic seeds (IEPOX, IEPOXOOH). JPAC conditions are closer to atmosphere than for example the ISOPOOH experiments which start from 60 ppb of ISOPOOH.<sup>76</sup> The JPAC chemical system is shifted towards RO<sub>2</sub>, but sufficient HO<sub>2</sub> - more than under atmospheric conditions - is available to provide sufficient ISOPOOH and thereby IEPOX as well as ISOP(OOH)O<sub>2</sub> and ISOP(OOH)<sub>2</sub>.

## Mass yields of key compounds and SOA formation potential

To assess the iSOA yields we converted the modelled gas-phase concentrations of the key compounds into gas-phase mass yields and compare them to the observed iSOA mass yields listed in Table S2 (Figure S12). Gas-phase mass yields of "SOA forming compounds" can be considered as maximal "potential" for iSOA formation wherein we will use the IEPOX mass yields to represent the iSOA formation potential for acidic seeds and the ISOP(OOH)<sub>2</sub> or HOM mass yields the iSOA formation potential for neutral seeds.

For the acidic seeds case we first note that the observed iSOA yields decrease with increasing isoprene consumption, just as the modelled IEPOX yield (Figure S12, upper panel). The experiments and the model result would be fully commensurable if 15-20% of gas-phase IEPOX eventually gets transferred to the seed particles. The reaction time in the RC is about one hour and that could be insufficient to generate the iSOA mass by liquid phase processes as observed

by other groups.<sup>8,35,74,85</sup> However, the iSOA IEPOX yields of 15-20% compare well with observed yields in a range from a few % up to10%,<sup>12,85,86</sup> if one takes into account that other gasphase compounds may also have contributed to iSOA mass (e.g. IEPOXOOH, ISOP(OOH)<sub>2</sub>, HOM). Wall loss effects on the yields are small since they have to compete with the condensation on the seed particles. The yields for iSOA on acidic aerosol in Figure S12 were wall loss corrected (see Table S2). As we will show below, our iSOA yield on acidic seeds of 4% leads to about same global burden of iSOA (37%) as MT-SOA (40%, excluding NO<sub>3</sub>-SOA contributions for both isoprene and MT) in our global model calculations in reasonable agreement with field observations (Table S5).



**Figure S12:** Comparison of the observed iSOA mass yields to the gas-phase mass yields of the major SOA-forming species IEPOX (blue, upper panel) for acidic seed, and isopene HOM (red, lower panel) and ISOP(OOH)<sub>2</sub> (orange) for neutral seed. For HOM we used two approaches, direct HOM in MCM (i.e. 9 compounds with  $O/C \ge 6/5$ ) and the result of an 1% branching to ISOP(OOH)<sub>2</sub> in the ISOPOOH + OH reaction, as proposed by D'Ambro et al.<sup>66</sup> Atmosphere like refers to [OH], [isoprene], and J values as defined in text. Gas phase mass yield can be considered as maximum "potential" of SOA formation by SOA-forming species.

In the neutral seed aerosol case the observed upper limit of the iSOA mass yield of 1% was in agreement with the estimate for ISOP(OOH)<sub>2</sub> or the prediction of HOM compounds by the actual MCM v3.3.1 mechanism (9 compounds with  $O/C \ge 6/5$ ). Note that we also observe only very minor isoprene HOM formation in our isoprene gas-phase experiments. However, the mass yield of ISOPOOH, and thus ISOP(OOH)<sub>2</sub> is decreasing with increasing consumption (decreasing [OH], Figure S11), while iSOA yields remained about stable. Recently, non-IEPOX pathways where described with mass yields of 4-15% at similar conditions.<sup>10</sup> At the moment we have no explanation for being closer to the low percentage values observed in previous studies.<sup>75,77,87,88</sup>

Overall we conclude that the concentrations of key species involved in iSOA formation in JPAC were commensurable with, or higher than, expectations for atmospheric conditions. To test our

findings we implemented SOA yields as determined in JPAC in the EMEP MSC-W model (next section 8).

# 8. Global modelling

The impact of OH scavenging and product scavenging is not limited to the  $\alpha$ -pinene & isoprene system as we showed above (section 5). Our laboratory studies were necessarily conducted at concentration levels deviating from those in the atmosphere. Additionally, transport and dilution of emission plumes were absent under the controlled laboratory conditions. We have shown that the concentrations of the main drivers in the isoprene SOA (iSOA) formation were not too far from typical atmospheric conditions in our experiments (previous section 7). In this section we will demonstrate by global modelling studies that OH scavenging and product scavenging can play a significant role under atmospheric conditions.

SOA	Fixed yields (FY)	References		
MT-OH-SOA	17%	JPAC, $\alpha$ -pinene, for all MT, Table S1		
MT-O <sub>3</sub> -SOA	17%	JPAC, $\alpha$ -pinene, for all MT, derived from the seeded dark experiments		
MT-NO <sub>3</sub> -SOA	0%for α -pinene30%for other MT	Fry et al. <sup>102</sup>		
SQT-SOA	17%	Mentel et al. <sup>103</sup>		
iSOA acidic seeds neutral seeds	4% ( <b>HI)</b> 1% (LI)	JPAC, upper limits, Table S2		
	Variable yields (VY)			
MT-OH-SOA	parametrised product scavenging	JPAC, $\alpha$ -pinene for all MT, Figure 2		

Table S4: Relevant SOA yields entering the global model calculations

Here we focus on SOA formed by monoterpenes oxidized by OH (MT-OH-SOA). This SOAproduction will respond directly to the OH scavenging and product scavenging that we have observed in the laboratory. In order to investigate the implications of these processes in the atmosphere we made use of the EMEP MSC-W chemical transport model v.4.13,<sup>43,44,89</sup> configured for global simulations and with a new SOA scheme for this study based on observed JPAC-yields where available (see Table S4). The gas-phase chemistry scheme used in the global modelling is based on an updated version of the CRI v2.5 mechanism<sup>90</sup> but with the isoprene chemistry replaced by a recently developed reaction scheme that describes the HOx recycling mechanism (included in MCM v3.3.1) in a simplified, but acceptable, way. The rates and products of the reactions in CRI v2.5 have been reviewed and updated to take into account new and revised IUPAC recommendations, and to be in line with MCM v3.3.1. For anthropogenic organic aerosols (OA) we use a simplified framework assuming non-volatile primary OA emissions (and no additional IVOC-emissions). SOA yields from aromatic VOC oxidation were adapted from Hodzic and co-workers.<sup>91</sup>

Because of very large uncertainties in SOA formation itself (e.g.<sup>1</sup>) and varying SOA representations in regional and global atmospheric models (e.g.<sup>92</sup>), we limit ourselves to demonstrating that OH scavenging and product scavenging can play a role in the real atmosphere under realistic conditions of transport, dilution and varying BVOC emissions. To comprehensively and robustly quantify the importance of OH-and product scavenging for the total biogenic SOA, it would be necessary to know for certain the fraction of all major BSOA components including those formed by the two other major oxidants in the atmosphere, O<sub>3</sub> (MT-O<sub>3</sub>-SOA) and NO<sub>3</sub> (MT-NO<sub>3</sub>-SOA). These fractions vary from model to model depending on the photochemical scheme, SOA yields, the condensation scheme etc. Moreover, since formation of MT-O<sub>3</sub>-SOA, SQT-SOA and even MT-NO<sub>3</sub>-SOA may also involve autoxidation as a major process, product scavenging may also lower the BSOA mass from these components. For this reason we consider our model approach as conservative. An additional large source of uncertainty lies in the BVOC emissions.<sup>93-96</sup>

The EMEP MSC-W model was run for 4% iSOA yield (HI) and 1% iSOA yield (LI) using three different model configurations – denoted 'NoIso', 'FY', and 'VY'. The NoIso run represents a reference case where the model was run with fixed SOA yields as given in Table S4, and with biogenic isoprene emissions switched off. The magnitude of the OH scavenging effect by isoprene was investigated in model runs with fixed yields (FY) for all SOA types including iSOA. This FY case represents the common assumption that SOA precursors do not interact chemically with each other and that production of SOA is additive. Finally, the product scavenging effect was considered by applying variable MT-OH-SOA yields (VY), depending on the instantaneous and local isoprene/MT consumption-ratio. The product scavenging considers that the presence of isoprene lowers the fraction of condensable HOM (LVOC and ELVOC) which can be formed from  $\alpha$ -pinene (and indeed all MT). In order to maintain consistency between the model representation based upon the observed relationship between relative yield and isoprene-to-monoterpene consumption ratios (Figure 2).

In order to evaluate the performance of the revised EMEP model with the implementations we have compared its predictions of organic aerosol against two well-established monitoring networks. Firstly, for Europe, we have used data from the EMEP monitoring network (www.emep.int<sup>97</sup>). These data, consist of either daily or weekly samples of organic carbon (OC), measured using a mixture of  $PM_{10}$  and  $PM_{2.5}$  filters. For the USA we have made use of OC data (in  $PM_{2.5}$ ) from the IMPROVE network (http://views.cira.colostate.edu/improve<sup>98</sup>). These two networks provide good quality data at rural sites across the respective regions. As we are

interested in the impacts of BVOC emissions, we here consider only data from the summertime period (Apr-Sep). To avoid mountain sites we restrict the analysis to sites with altitude < 500 m. Results for the HIFY and HIVY cases were almost identical, so we present only the HIVY case here.

Figure S13 compares the summertime OC results from both networks. For Europe (Figure S13a), the model shows a good correlation with the measurement sites (R=0.64), though under-predicts by a factor of about 2 for the more polluted sites. For the USA (Figure S13b) the match between modelled and observed OC is remarkably good, with R=0.84 and almost a 1:1 relationship. Given the significant difficulties usually seen when comparing modelled versus observed carbonaceous aerosol (e.g.<sup>92</sup>), driven by uncertainties in precursor emissions, formation and loss mechanisms, these results are very satisfactory, and provide some confidence that the SOA yields used in this study are broadly consistent with atmospheric conditions.



**Figure S13:** Comparison of modelled versus observed OC concentrations in Europe (panel a) and USA (panel b). Modelled data are from the 'HIVY' setup. European data are from the EMEP network, USA data from the IMPROVE network, see text. Data are averages from April-Sept. 2012, for sites below 500m altitude. The grey shading indicates the number of observations that were included in the comparison for the individual sites. The 1:1 line is given in green.

Table S5 shows that in the HIFY case MT-OH-SOA contributed about 20% to both the total BSOA burden (mass) and the BSOA concentration in the lowest model layer. In the surface layer the model simulated contributions to BSOA were fairly similar (15-24%) for the five classes: MT-OH-SOA, MT-O<sub>3</sub>-SOA, MT-NO<sub>3</sub>-SOA, iSOA and SQT-SOA.

Consistent with our JPAC experiments, inclusion of isoprene (emissions) in the model calculations substantially lowers the OH concentration (Figure S14, top). The effect is most evident in regions of high isoprene emissions such as the tropical forests in South America and

Africa. This shows that isoprene is co-controlling the available OH (compare<sup>19</sup>) and OH scavenging by isoprene could indeed be a substantial factor influencing MT oxidation and subsequent BSOA formation in the tropics. However, as can be also seen in Figure S14 (top), some regions exist where isoprene emissions lead to substantial increases in the modelled OH concentrations, most notably in large parts of eastern China and some areas in North America – the common feature of these regions seems to be high NOx concentrations in combination with relatively low to moderate isoprene levels in the model simulations.

SOA fractions (FY)	Global Burden	Global Surface Concentration		
MT-OH-SOA	21%	20%		
MT-O <sub>3</sub> -SOA	19%	24%		
iSOA (yield 4%)	37%	24%		
MT-NO <sub>3</sub> -SOA	11%	16%		
i-NO <sub>3</sub> -SOA	3%	2%		
SQT-SOA	9%	15%		

Table S5: Detailed fractions of biogenic SOA on global scale

The lower OH concentrations caused by isoprene OH scavenging are reflected in the strong decreases in MT-OH-SOA shown in Figure S14 (middle). Note, that only the linear mixing effect according Eq. 5 is considered in a fixed yield approach. A dependence of the yield on OH itself and the impact of gas/particle partitioning of semi-volatile OC (Raoult's Law effect) would further decrease MT-OH-SOA. Again the OH scavenging effect is strongest in the tropical regions, with a MT-OH-SOA reduction by 40% in South America (Figure 5). The effect should be most important in areas with sufficiently strong MT emissions in the presence of isoprene emissions. The difference plot shows that these conditions are found in tropical regions, but some effect is also seen in a wide range of temperate regions in the Northern Hemisphere (Figure S14, bottom). We conclude that OH scavenging by isoprene should lead to reduced formation of MT-OH-SOA also in a world with varying emissions, realistic isoprene/BVOC ratios, transport and dilution. On a global scale the model calculations predict surface-layer MT-OH-SOA decreases by 25% due to isoprene (Figure 5; Global). The OH scavenging effect is largest in regions with high isoprene emissions, whether densely populated (South East Asia, North America) or not (South America, South Africa). The effect is smaller in regions with low isoprene emission such as Russia and Western Europe.



**Figure S14:** Effect of OH scavenging on MT-OH-SOA. Top: Ratio of the OH concentration in a world without (NoIso) and with isoprene (HIFY). Middle: Lower OH concentrations in the presence of isoprene emissions indeed reduce the MT-OH-SOA mass concentration significantly. Bottom: without OH scavenging effect by isoprene the MT-OH-SOA would be larger by up to  $1 \ \mu g/m^3$  in tropical regions and in the South East USA and up to  $0.1 \ \mu g/m^3$  in wide temperate areas (lower panel).

MT-OH-SOA is even further reduced when the *product scavenging effect* is implemented in the model (HIVY). Product scavenging reduces MT-OH-SOA (HIFY) predictions further by 10%-30% in most regions of the world; over the isoprene emitting tropical forests in South America and Africa the reduction can be >50% (Figure S15, top).

The modelled total effect of OH scavenging and product scavenging by isoprene is a reduction of MT-OH-SOA by 40% on the global scale (Figure 5). The scavenging effect is largest in regions with high isoprene/MT like South America with a reduction of 55% and South East Asia (45%)

and smaller in regions with lower isoperene/MT like Russia and Western Europe with reductions of 28% and 19%, respectively (Figure 5).

It should be noted that OH scavenging by isoprene increases the importance of  $MT-O_3$ -SOA (Figure 5, orange). The increase of the  $MT-O_3$ -SOA compensates the OH scavenging effect to some extent when the sum of MT-OH-SOA and MT-O\_3-SOA (= MT-Ox-SOA, sum of red and orange bars in Figure 5) is considered. However, the reduction of MT-OH-SOA due to product scavenging still leads to significant (up to 20%) reductions of the total MT-Ox-SOA over large regions despite the compensating formation of MT-O\_3-SOA (blue areas Figure S15, bottom).

Our approach is conservative. We note, that in the model calculation the iSOA production is larger than the OH scavenging and product scavenging effects for an iSOA yield of 4 %, which assumes acidic aerosol everywhere (Figure 5, sum of brownish bars). If the iSOA is formed at 1% yield (neutral aerosols) the net effect of the isoprene emissions on BSOA concentrations may even be negative in some regions (Figure 5, Western Europe).



Figure S15: Effect of product scavenging as determined in this study on MT-OH-SOA (top) and on MT-Ox-SOA = MT-OH-SOA + MT-O<sub>3</sub>-SOA (bottom). The increase in MT-O<sub>3</sub>-SOA is not sufficient to compensate the reduction of MT-OH-SOA by the product scavenging effect.

We further note that e.g. MT-O<sub>3</sub>-SOA also has a significant contribution of autoxidation products including HOM monomers and dimers.<sup>22</sup> During daytime isoprene could reduce the MT-O<sub>3</sub>-SOA production by scavenging HOM peroxy radicals from MT ozonolysis. If we assume a similar reduction, the compensation effect by MT-O<sub>3</sub>-SOA would be reduced. Assuming an additional product scavenging effect for MT-O<sub>3</sub>-SOA as for MT-OH-SOA and applying the low iSOA yield (1%) would already lead to a (small) net reduction of the BSOA mass (PSOx, Figure 5). The same arguments may also hold for HOM-peroxy radicals from SQT (ozonolysis and reaction by OH) and SQT-SOA.

In summary, the model calculations clearly suggest that the OH scavenging effect (by isoprene) is significant in the real environment. The product scavenging leads to an additional substantial reduction of the MT-OH-SOA fraction. The reduction is still significant when all MT-Ox-SOA is considered although the OH scavenging effect is partly compensated by a gain in MT-O<sub>3</sub>-SOA. To assess the overall importance of OH scavenging and product scavenging, we must assess the ratio of MT-OH-SOA to all other BSOA-components and the product scavenging in day time ozonolysis (MT-O<sub>3</sub>-SOA) and NO<sub>3</sub> reactions (MT-NO<sub>3</sub>-SOA) in the night. However, the impact of product scavenging on MT-O<sub>3</sub>-SOA and MT-NO<sub>3</sub>-SOA has not been determined yet and overall SOA-yields and model implementations for SOA vary widely<sup>92</sup> and currently we are not able to estimate the different SOA fractions with sufficient accuracy.

## 9. Wall effects

Wall loss in simulation chambers is currently heavily debated.<sup>22,31,27-30</sup> Note that JPAC is a continuously stirred flow reactor made of borosilicate glass, operated with residence times of about 50 min (Volume 1450 L, Flow 30 L/min). A fan ensures fast mixing (minute) and as a consequence the core of the reactor is always well mixed despite the losses to the walls which occur by diffusion through the laminar boundary layer near the walls. Diffusive loss is mass and size dependent and thus different for HOM monomers, HOM dimers, and aerosol particles. Details of the wall losses of HOM were described previously.<sup>22,31</sup> In short: chamber lifetimes of photochemically generated HOM with very low vapour pressures were determined by measuring their decay rate in the chamber after the UV-light and thus the OH production was turned off. Typically, decay rates were first order and lifetimes were of the order of 10<sup>2</sup> s for HOM compared to 10 min for particles with diameters of 1.5 - 7 nm<sup>99</sup> and 50 min for larger particles with 60-70 nm diameters. The lifetimes of the latter are similar to the residence time in the chamber, i.e. they are mainly flushed out.<sup>46</sup> From the determination of lifetimes for HOM in the particle free chamber we derive the set of wall loss coefficients Lw<sub>HOM</sub> for individual HOM.

In the presence of aerosol particles, either photochemically produced by new particle formation or by adding seed aerosols to the chamber, condensation of HOM onto particle surfaces competes with the wall losses. Due to the additional loss of HOM by condensation to particles with coefficient  $Lp_{HOM}$  the presence of particles shortens the lifetime of gaseous HOM(g) in the chamber (Eq. 6).

$$\tau_{HOM} = \frac{1}{L_{HOM}} = \frac{1}{L_{WHOM} + L_{PHOM}} \tag{6}$$

With increasing particle surface, condensation onto particles competes more and more with the wall losses and eventually most of the HOM condense on particles and form SOA. The latter is the desired situation for determining SOA mass and SOA yields. For example, the lifetime of the HOM  $C_{10}H_{16}O_7$  decreases in presence of increasing amount of particles, i.e. increasing particle surface from 150 s in the particle free chamber to about 20 s at a surface density of  $5 \times 10^{-4} \text{ m}^2/\text{m}^3$  (Figure S16).  $C_{10}H_{16}O_7$  and the particles were generated by photooxidation experiments with increasing amounts of  $\alpha$ -pinene. Surface densities were calculated from measurements of the number size distribution by the SMPS.  $C_{10}H_{16}O_7$  is one of the largest signals in the mass spectra and as for the wall losses in the particle free chamber, the lifetime of  $C_{10}H_{16}O_7$  was determined directly from the decay rate of  $C_{10}H_{16}O_7$  after switching off the UV source and thus OH. Such direct measurements of lifetimes required time resolutions <10 s and many HOM signals were too weak to allow reliable determinations of decay rates at such time resolution.



**Figure S16**: Lifetimes of  $C_{10}H_{16}O_7$  as a function of increasing particle surface. Particles were produced by photooxidation of  $\alpha$ -pinene at different  $\alpha$ -pinene concentrations. The  $C_{10}H_{16}O_7$  is a HOM product of  $\alpha$ -pinene photooxidation. The lifetime was determined by analysing the decay rates of the signal of  $C_{10}H_{16}O_7$  when the UV source, i.e. the OH source, was switched off. Errors of lifetimes were estimated to  $\pm 20$  %, those of particle surfaces to  $\pm 10\%$ . The dashed black line shows the life times calculated by eq. 6 with  $Lw_{HOM} = 1/150 \text{ s}^{-1}$  and eq. 13 with  $\gamma$ =1,  $f_{FS}$ =1, and  $\bar{\nu} = 156 \text{ m/s}$ )

We therefore applied measurements at steady state conditions with increasing amount of ammonium seed aerosols allowing for the integration of HOM signals over several minutes. In steady state the concentration of a HOM,  $c_{HOM}$ , is given by the gas-phase production rate of HOM  $P_{HOM}$  divided by the total loss coefficient of HOM  $L_{HOM}$  - or multiplied by the lifetime of HOM  $\tau_{HOM}$  in the chamber (Eq. 7).  $P_{HOM}$  was held constant by keeping the concentrations of the

VOC,  $O_3$  and OH constant.  $L_{HOM}$  which is given by the sum of loss coefficients for wall losses  $Lw_{HOM}$  (neglecting the loss by flush out) and for condensation onto particles  $Lp_{HOM}$ , was varied by adding different amounts of seed aerosols.

$$C_{HOM} = \frac{P_{HOM}}{L_{WHOM} + L_{PHOM}} = P_{HOM} \cdot \tau_{HOM}$$
(7)

We normalize the experiments with seed aerosols to the case of the particle free chamber at otherwise the same boundary conditions (indicated by superscript 0);  $c_{HOM}/c_{HOM}^{0}$  is then given by Eq. 8, wherein  $P_{HOM}$  cancelled out.

$$\frac{c_{HOM}}{c_{HOM}^0} = \frac{\tau_{HOM}}{\tau_{HOM}^0} = \frac{Lw_{HOM}}{Lw_{HOM} + Lp_{HOM}}$$
(8)

Since we are far away from saturating our mass spectrometric signals, the signal intensity is directly proportional to the concentration of the respective HOM allowing for replacing  $c_{HOM}$  by  $\alpha \cdot S_{HOM}$  wherein  $S_{HOM}$  is the signal intensity measured for a given HOM and  $\alpha$  is the respective calibration factor of the NO<sub>3</sub><sup>-</sup>-CIMS. In replacing  $c_{HOM}$  by  $\alpha \cdot S_{HOM}$  we achieve Eq. 9 wherein the calibration factor  $\alpha$  cancelled out.

$$\frac{S_{HOM}}{S_{HOM}^0} = \frac{L_{WHOM}}{L_{WHOM} + L_{PHOM}} \tag{9}$$

Note  $S_{HOM}/S_{HOM}^{0}$  is just the branching ratio into wall loss, i.e. gives the fraction of a HOM which sticks onto the wall.

We can now determine the loss to particles from the determination of  $Lw_{HOM}$  and the signal ratio  $S_{HOM}^{0/0}/S_{HOM}$  for given total particle surface  $S_{tot}$  (Eq. 10).

$$Lp_{HOM} = \frac{S_{HOM}^0}{S_{HOM}} \cdot Lw_{HOM} - Lw_{HOM}$$
(10)

The branching ratio into condensation i.e. the fraction of HOM ( $Fp_{HOM}$ ) that form SOA is then given by Eq. 11.

$$Fp_{HOM} = \frac{Lp_{HOM}}{Lw_{HOM} + Lp_{HOM}} = 1 - \frac{S_{HOM}}{S_{HOM}^0}$$
(11)

As  $Lp_{HOM}$  depends on the actual particle surface,  $Fp_{HOM}$  also depends on the actual particle surface. At negligible small particle surface ( $Lw_{HOM} >> Lp_{HOM}$ ) all HOM are lost on the walls of our chamber. At high particle surface ( $Lp_{HOM} >> Lw_{HOM}$ ) losses of HOM on the chamber walls would be negligible.

Eq. 11 is valid for each individual HOM and for the total effect one would have to integrate over all HOM. However, in the following we will show that  $Fp_{HOM}$  will give a general correction function independent of the individual HOM. Moreover, it is valid for low volatility HOM (LVOC-HOM) if we assume that -cum grano salis - the same organic matrix is formed on the glass walls of the reactor and on the surface of seed particles. Note in this context that  $\alpha$ -pinene SOA forms films on the surface even of aqueous ammonium sulfate seed aerosols,<sup>100</sup> i.e. indeed a two phase system with a separated organic phase.

 $Lw_{HOM}$  is governed by diffusion through a stagnant boundary layer at the chamber walls.  $Lw_{HOM}$  is thus proportional to the diffusion constant of HOM  $Dg_{HOM}$  and the inner surface area of the chamber Sw (7.08 m<sup>2</sup>) and inverse proportional to the thickness (l) of the diffusive boundary layer (eq.12).

$$Lw_{HOM} = \gamma \cdot \frac{Dg_{HOM}}{l} \cdot Sw \tag{12}$$

In Eq. 12 Dg<sub>HOM</sub> is proportional to the mean molecular speed  $\bar{v}$  and the mean free path  $\lambda_{HOM}$ . The uptake coefficient  $\gamma$  accounts for the fact that not every collision with the surface leads to uptake at the walls or particles (see below). Transport to the particle surface is eventually also a diffusive process. The Lp<sub>HOM</sub> can be approximately described by the collisions of HOM with the total particle surface Sp<sub>tot</sub> (Eq. 13).

$$LP_{HOM} = \gamma \cdot f_{FS} \cdot \frac{\bar{\nu}}{4} \cdot Sp_{tot}$$
(13)

In Eq. 13  $f_{FS}$  is the Fuchs-Sutugin factor<sup>101</sup>, which is a function of the ratio of  $\lambda_{HOM}$  and the particle radius and interpolates between the two boundary conditions *gas-kinetic regime* and *continuous diffusion regime*. We calculated  $f_{FS}$  to be always larger than 0.85 for our experimental conditions.

Let us assume that in steady state we indeed formed the same organic matrix in particles and on the walls, which means that  $\gamma$  is same for both processes. The only specific molecular property in Eq. 11 and Eq. 12 is then the  $\bar{v}$  which depends on the square root of the inverse molecular weight. However,  $\bar{v}$  cancels out in Eq. 11 and thus Fp<sub>HOM</sub> will be the same for each HOM.

We verified our approach by measuring the formed SOA mass by AMS in seeded experiments. SOA mass generated from  $\alpha$ -pinene or  $\beta$ -pinene under different reaction regimes (NO<sub>X</sub>) shows the same functional dependence on the surface of the seed aerosol (Figure S16). If we assume that SOA is essentially formed by HOM which are ELVOC, we can neglect evaporation from the walls and particles with respect to the chemical production and calculate the fraction condensing onto particles (compared to fraction sticking to the walls by Eq. 12). Fp<sub>HOM</sub> was calculated by using Lw<sub>HOM</sub> =  $1/\tau_{HOM}$  and Eq. 13 with  $\gamma$ =1 and f<sub>FS</sub>=1 in the chamber. Fp<sub>HOM</sub> curve is shown in Figure S17, it matches functionality of the observations very well. Moreover, dividing the observed organic mass by Fp<sub>HOM</sub> will correct exactly for the SOA mass which was deposit on the walls. We conclude that our method of wall loss corrections is based on fundamental principles and we can reduce it to direct observations, i.e. the ratio of S<sub>HOM</sub>/S<sub>HOM</sub><sup>0</sup> in the particle loaded and particle free chamber.



**Figure S17:** Organic mass as a function of increasing particle surface provided by seed particles. Production rates of HOM were held constant and seed particle concentrations were changed by flush out after stopping seed addition. If scaled, SOA formed by photooxidation of  $\alpha$ -pinene at low NO<sub>X</sub> (red open circles, left y-scale) and  $\beta$ -pinene at high NO<sub>X</sub> (blue filled circles, right y-scale) show the same dependence on the particle surface. ([ $\alpha$ -pinene]/[NOX] ~ 33 ppbC·ppb<sup>-1</sup>), [ $\beta$ -pinene]/[NOX] ~ 1.8 ppbC·ppb<sup>-1</sup>). The maximum load of ammonium sulfate seed particles was 88.5 µg m<sup>-3</sup>; the number distribution was polydisperse, but monomodal with a mean diameter ~ 70 nm.

By definition  $Fp_{HOM}$  ranges from 0 to 1, and the axes were arranged for direct comparison with the measured data points. The black line shows  $Fp_{HOM}$  calculated for the HOM  $C_{10}H_{16}O_7$  with molecular weight of 248 g/mol,  $\bar{\nu} = 156$  m s<sup>-1</sup> for a wall loss rate = 0.0067 s<sup>-1</sup> equivalent to a HOM lifetime of 150 s (compare Figure S16), uptake probability  $\gamma = 1$ , Fuchs-Sutugin factor  $f_{FS} = 1$ . The dashed dotted line shows that the effect of  $f_{FS}$  would be hardly detectable for  $1>f_{FS}>0.75$  in Lp<sub>HOM</sub>. For molecules with molecular formulas  $C_{10}H_{16}O_{4-12}$  and 70 nm particles  $f_{FS} > 0.85$  and neglection of  $f_{FS}$  causes only small effects. If LVOC-HOM with substantial vapour pressures<sup>39,72</sup> are involved in SOA formation, the evaporation would manifest in such that  $Lw_{HOM}$  and  $Lp_{HOM}$  become net fluxes under our steady state conditions. This would simple become manifest in  $\gamma < 1$ . However, with the assumption of the same organic matrix on walls and particles, the  $\gamma$  cancel out and the same Fp also applies for LVOC-HOM. We therefore applied the correction Fp<sub>HOM</sub> shown in Figure S17 to all our yield data.

Most experiments were performed at  $S_{tot} > 6 \cdot 10^{-4} \text{ m}^2 \text{ m}^{-3}$ , i.e. the corrections applied were less than 30%. In some case with  $S_{tot} < 0.4 - 0.1 \text{ m}^2 \cdot \text{m}^{-3}$  corrections from 1.5 to 2 were applied. A list of all applied correction factors is found in Table S1. The data were obtained at particle surface densities between  $1.3 \cdot 10^{-4}$  to  $1.9 \cdot 10^{-3} \text{ m}^2 \text{ m}^{-3}$ . This led to correction factors  $1/\text{Fp}_{\text{HOM}}$  in the range between 1.1 and 2.4. The variation of  $1/\text{Fp}_{\text{HOM}}$  was mainly caused by varying amounts of seed aerosol added during individual experimental runs. Within the experiment sets e.g.  $\alpha$ -pinene alone (Table S1, top) or  $\alpha$ -pinene&isoprene mixtures (Table S1, bottom),  $1/\text{Fp}_{\text{HOM}}$  varied much less as the generation of seed particles by the atomizer was quite constant. Addition of isoprene to the  $\alpha$ -pinene reaction system increased  $1/\text{Fp}_{\text{HOM}}$  as the organic mass was reduced by the isoprene addition and therewith also the total particle surface. Removing isoprene from the reaction systems decreased  $1/\text{Fp}_{\text{HOM}}$  because the organic mass and the size of the particles increased again. This shows that the net effect of isoprene, i.e. the OH scavenging effect and the product scavenging effect, would have been overestimated if the data would not have been corrected for the wall losses of the HOM.

However, due to the application of seed particles the changes in  $Fp_{HOM}$ , and thereby the changes in the correction factors were not very large. For the lowest particle surface used in these experiments,  $1/Fp_{HOM}$  increased from 1.77 to 2.4 i.e. by roughly 35% due to the isoprene addition. In all other cases the values of  $1/Fp_{HOM}$  increased by less than 16% when isoprene was added (see Table S1). We estimate the error caused by the correction procedure to ~20% for the lowest particle surface and to ~10% for the other data points<sup>20</sup>. Uncertainties in  $1/Fp_{HOM}$  were therefore much lower than the effect of isoprene on mass formation.

Organic products deposited on the walls can also act as source for SOA, if they evaporate and condense onto the seed aerosols. This will happen when fresh seed aerosol is added to the chamber and perturbs the wall gas-phase equilibrium by condensation of gaseous components. We quantified potential transfer of SOA material from the walls to the seed aerosols by switching off the VOC source in the RC while keeping the oxidants O<sub>3</sub> or OH in place. The condensation of organic material of seed aerosols was monitored by AMS. (The results are partly positively biased by AMS, as AMS analysis a priori accounts unassigned signals to organics.)

During ozonolysis wall products generated  $0.5 - 1.5 \ \mu g/m^3$  SOA This contribution is relatively small (10% of maximum SOA) and stable, because products emerging from the walls cannot be further oxidized by ozone. If UV is turned on and OH is available, more SOA was produced on the seed aerosols as wall products can now be further oxidized leading to lower vapour pressure products. In the case of neutral ammonium sulfate the OH/wall product contribution after 60 h of

experiment was increased from 1.5 to 2.8  $\mu$ g/m<sup>3</sup>. [OH] was two times higher than in presence of  $\alpha$ -pinene, which leads to an overestimation of the wall effect to the SOA mass observed during the core of the experiment.

The situation is different in the presence of acidic ammonium bisulfate aerosols. Here we measured 1.6  $\mu$ g/m<sup>3</sup> of OH-wall contribution before the core experiment. The OH-wall contribution increased in the course of the experiment to about 4  $\mu$ g/m<sup>3</sup> over 40 h. We attribute this increase to deposition of ammonium bisulfate particles which slowly acidified the walls and mobilized an increasing amount of acidic organic components. Again [OH] was 1.6 times higher than in the presence of  $\alpha$ -pinene overestimating the true effect during the core experiments.

Note that the SOA baseline caused by wall deposits and their oxidation products will counteract the isoprene effect and makes our observations of the isoprene effects a lower limit. We therefore did not correct for the wall produced SOA, but subsumed the baseline effects under the error of our SOA yields.

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